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## Impact of Cold Chain and Product Variability on Quality Attributes of Modified Atmosphere Picked Mushrooms (*Agaricus bisporus*) Throughout Distribution

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1 **IMPACT OF COLD CHAIN AND PRODUCT VARIABILITY ON QUALITY**  
2 **ATTRIBUTES OF MODIFIED ATMOSPHERE PACKED MUSHROOMS (*Agaricus***  
3 ***bisporus*) THROUGHOUT DISTRIBUTION**

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13

14 **ABSTRACT**

15 An integrated mathematical modelling approach was followed to model the heat and mass  
16 transfer processes taking place in modified atmosphere packaged mushrooms and its effect on  
17 the quality throughout distribution supply chain was simulated. The model equations were  
18 solved to obtain the concentration of gases (O<sub>2</sub>, CO<sub>2</sub>) and H<sub>2</sub>O in the headspace of the  
19 package. The change in the quality (colour and weight loss) during the distribution supply  
20 chain were monitored. The simulation results are in agreement with the experimental data.

21 The model can study the effect of biological parameters and cold chain parameters on the  
22 quality of mushroom. Weight loss is influenced by the cold chain parameters whereas product  
23 lightness (L) value is influence by the product uncertainty parameters. Sensitivity analysis  
24 was performed to quantify the effect of individual parameters on the quality of mushroom.

25 Using this integrated model the changes in the quality of MAP mushroom during the supply  
26 chain can be predicted and the losses can be assessed at each step.

## 27 **1. Introduction**

28 Mushrooms are highly perishable produce because of the absence of a cuticle to protect them  
29 from mechanical damage, microbial attack and quality loss. Susceptibility of mushroom to  
30 microbial attack and enzymatic browning is due to its high respiration rates and high moisture  
31 content (Aguirre et al., 2008; [Oliveira et al., 2012](#)). The shelf life of mushroom at ambient  
32 temperature is 1-3 days. Managing the supply chain is challenging as its quality deteriorates  
33 significantly over time at rates dependent on temperature and relative humidity (Blackburn  
34 and Scudder, 2009). Modified atmosphere packaging (MAP) is a postharvest technique used  
35 to increase the shelf-life of fresh produce, it also responds to the emerging consumer demand  
36 for convenience and quality. MAP alters the atmosphere inside package, it relies on transfer  
37 of gases through packaging film which leads to atmosphere rich in CO<sub>2</sub> and deficient in O<sub>2</sub>  
38 ([Oliveira et al., 2012](#)).

39 Modified atmosphere packaging of mushrooms accompanied with low temperature storage is  
40 effective in extending the shelf life and retards quality changes (Cliffe-Byrnes and O'Beirne,  
41 2007). Concentrations of CO<sub>2</sub>>12 % can result in quality degradation due to browning and  
42 concentration of O<sub>2</sub><1% leads to anaerobic respiration resulting in off flavour production and  
43 susceptibility to microbial contamination ([Kim et al., 2006](#); [Tano et al., 2007](#); [Villaescusa and  
44 Gil, 2003](#)). The optimum conditions reported for shelf life extension of mushroom is 2.5 –  
45 5% CO<sub>2</sub> and 5-10% O<sub>2</sub> stored at 2<sup>0</sup> C (Ares et al., 2007). The use of microperforated films  
46 has been widely reported to prevent the accumulation of CO<sub>2</sub> and depletion of O<sub>2</sub> within the  
47 package and prevention of condensation. Temperature has a major effect on the rate of  
48 metabolic processes taking place in mushroom, its dependence on respiration rate and  
49 permeability should be taken into account for designing an ideal MA package (Charles et al.,

50 2005). Mushrooms have high sensitivity towards relative humidity because they lack a barrier  
51 against diffusion. Saturated in-package conditions can lead to condensation on the produce  
52 surface and walls which can favour microbial growth and browning (Oliveira et al., 2012;  
53 Roy et al., 1995). Thus, water permeable films are recommended to be used for packaging  
54 mushrooms to reduce waste due to spoilage during the distribution chain.

55 Quality characteristics of mushroom are visual appearance, colour, freshness, microbial  
56 growth, weight loss (Aguirre et al., 2008). Quality evolution is predominately affected by the  
57 storage conditions including temperature and relative humidity. The main processes leading  
58 to waste generation are browning and textural changes. Texture changes can be caused from  
59 the weight loss due to moisture loss (Lukasse and Polderdijk, 2003). Weight loss observed in  
60 open mushroom punnets stored at 5<sup>0</sup> C is averaged at 4 % per day (Mahajan et al., 2008).

61 All fresh produce possesses a large inherent variability. Management of its biological  
62 variability is challenging for industries. The variability is controlled as much as possible by  
63 sorting and grading the product after harvest (Hertog et al., 2004). During storage the  
64 individual produce shows the same generic behaviour, however the variation can be observed  
65 due to the time zero from which the product is being observed. Variation during storage  
66 would be negligible if all the produce was harvested at same biological age (Hertog, 2002).  
67 This would make deciding upon the acceptability of a batch easy as all produce will show  
68 same quality characteristics. However, mushrooms are not harvested with such homogeneity  
69 therefore some items will degrade sooner than the others.

70 Distribution supply chain refers to a sequence of activities performed in order to deliver the  
71 highest quality fresh produce from the farm to the consumer (Tijskens et al., 2001). During  
72 the distribution supply chain the environmental conditions and the product itself has the  
73 potential to influence its quality. Management of uniform quality throughout the distribution  
74 supply chain is strenuous as mushrooms are affected by the biological variance and ignoring

75 these biological variances can lead to misleading conclusions. The major challenge is to  
76 develop a predictive model that takes into account the uncertainty of the predicted results  
77 (Hertog et al., 2007). Biophysical properties of the skin, mass transfer coefficients, initial  
78 value of colour (L, a and b value), respiration rate parameters have been identified as  
79 variables affecting the quality of mushroom in cold chain supply (Mahajan et al., 2008;  
80 Sastry and Buffington, 1983). Understanding the mechanism and dynamics of variation will  
81 eventually result in better prediction of the changes in the quality and losses observed during  
82 distribution supply chain.

83 Thus, the main objective of this study was to develop a model to study the effect of MAP  
84 design parameters on product quality and to assist in identifying where the waste is generated  
85 during distribution. To assess the effect of the cold chain factors (temperature and relative  
86 humidity) and the biological factors on the quality of mushroom in modified atmosphere  
87 packaging during distribution. Sensitivity analysis was performed to quantify the effect of  
88 biological parameters on the quality of mushroom.

## 89 **2. Mathematical model**

90 Mathematical modelling captures the useful properties of a food system. In this section, we  
91 outline the governing ordinary differential equations and other equations that describe the  
92 metabolic activity (respiration, transpiration), the transport of gas taking place through  
93 permeable films and perforations, dimensions of a package and changes in quality (L, a and b  
94 value, browning index and weight loss) during storage.

### 95 **2.1. Model hypothesis**

- 96 1. The material and energy balances arising from MAP packaging of mushrooms may be  
97 described using a compartmental model and lumped transfer coefficients.
- 98 2. O<sub>2</sub> consumption and CO<sub>2</sub> production due to respiration may be described by a  
99 Michalies-Menten type model with uncompetitive inhibition of CO<sub>2</sub>.

- 100 3. Package walls are impermeable and perforated film is permeable to O<sub>2</sub>, CO<sub>2</sub>, N<sub>2</sub> and  
 101 H<sub>2</sub>O.
- 102 4. Packaged produce and the gases inside package are in thermal equilibrium.
- 103 5. The surface of the mushroom is assumed to be saturated (water activity≈1).
- 104 6. Condensation of water may occur in the product or the package when the free volume  
 105 air relative humidity reaches 100% using a saturated surface model.
- 106 7. The quality of the mushroom colour maybe described using the temperature and  
 107 relative humidity model from (Aguirre et al., 2008) together with the relative  
 108 extension approach from (Hertog, 2002).

## 109 2.2. Mass Balance

### 110 2.2.1 Gas exchange in package

111 The quantities of gases change dynamically in the headspace of the package during storage.  
 112 The mass balance of gas components in the package is represented by ordinary differential  
 113 equations (Song et al., 2002). This model includes the convective gas transfer through the  
 114 packaging film including perforations and concentration of gas inside and outside of the  
 115 package and the rate of O<sub>2</sub> consumption and CO<sub>2</sub> production. (Oliveira et al., 2012) used this  
 116 model for MAP packaging of fresh sliced mushroom.

$$117 V_f \frac{d[O_2]_i}{dt} = 100 \times \left[ \frac{A_{p1} P_{O_2} P_{atm}}{L_f} \left[ \frac{[O_2]_o}{100} - \frac{[O_2]_i}{100} \right] - W_s r_{O_2} \right] \quad (1)$$

$$118 V_f \frac{d[CO_2]_i}{dt} = 100 \times \left[ \frac{A_{p1} P_{CO_2} P_{atm}}{L_f} \left[ \frac{[CO_2]_o}{100} - \frac{[CO_2]_i}{100} \right] + W_s r_{CO_2} \right] \quad (2)$$

119 As the package initially contains air, initial conditions (t=0) becomes [O<sub>2</sub>]<sub>i</sub>= =21.0%,  
 120 [CO<sub>2</sub>]<sub>i</sub>=0.03% and V<sub>f</sub> (ml) free volume is the difference between the pack volume and bulk  
 121 volume of mushroom.

### 122 2.2.2. Film water permeation

123 The driving force of water vapour permeation from the headspace of the package to the  
124 surrounding is the water vapour pressure difference (Becker and Fricke, 1996a) . The rate of  
125 water permeated from the headspace of package through the film can be calculated using Eq.  
126 (3).

$$127 \frac{dm_{pr}}{dt} = \left[ \frac{P_{H_2O} A_p (p_i - p_o)}{L_f} \right] \left[ \frac{0.018 P_{atm}}{RT_s} \right] \quad (3)$$

### 128 2.2.3. Humidity Ratio

129 The humidity ratio can be calculated from the mass balance to water vapour in the package  
130 headspace, considering the transpiration rate  $t_r$  of the product, the water permeated through  
131 the film  $m_{pr}$  and the total mass of headspace air (Jalali et al., 2017; Song et al., 2002))

$$132 \frac{dHR}{dt} = \frac{t_r - m_{pr}}{W_a} \quad (4)$$

133 Using Eq. (4), the relative humidity in the headspace can then be estimated as the ratio of the  
134 humidity ratio inside the package at any time (eq. 4) to the humidity ratio of saturated water  
135 vapour ( $HR_{sat}$ ) at the same temperature Eq. (5) (Becker et al., 1996).

$$136 HR_{sat} = \frac{0.62198 p_s}{(P_{atm} - p_s)} \quad (5)$$

### 137 2.3. Heat Balance

138 The temperature of surface of produce and gases surrounding it in headspace is assumed to be  
139 uniform. The major source of heat generation inside the MAP is respiration heat by fresh  
140 produce and heat is transferred in headspace due to convection, transpiration and  
141 condensation. Thus, overall energy balance in the package is written as follow.

$$142 Q_r W_s + Q_{con} + h_p A_p (T_o - T_i) = Q_{tr} + W_s C_s \frac{dT_s}{dt} + W_a C_a \frac{dT_s}{dt} \quad (6)$$

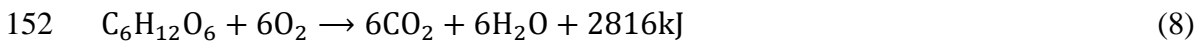
143 This equation can be simplified to obtain rate of temperature change inside package ( $T_s$ ).

$$144 \frac{dT_s}{dt} = \frac{Q_r W_s + Q_{con} + h_p A_p (T_o - T_i) - Q_{tr}}{W_s C_s + W_a C_a} \quad (7)$$



145 **2.3.1. Metabolic process**

146 Respiration is a metabolic process which provides energy for the biochemical processes  
147 occurring. The respiration rate also acts as an indicator of the shelf life of fresh produce, with  
148 mushrooms having a relatively high respiration rate and thus a short shelf life. MAP reduces  
149 the respiration rate of produce, increasing shelf life and maintaining quality (Cliffe -Byrnes  
150 and O’Beirne, 2007). During this process energy is generated, part of which is released as  
151 heat (Eq. 8) (Becker and Fricke, 1996b; Fonseca et al., 2002).



153 **2.3.1.1. Respiration Rate**

154 In this work O<sub>2</sub> consumption rates ( $r_{O_2}$ ) and CO<sub>2</sub> production rates ( $r_{CO_2}$ ) are calculated from  
155 the Michaelis-Menten enzyme kinetics model with uncompetitive type CO<sub>2</sub> inhibition. The  
156 rate of CO<sub>2</sub> production and O<sub>2</sub> consumption is a function of temperature, thus temperature  
157 dependence is studied using Arrhenius equation (Iqbal et al., 2009; Lu et al., 2013).

158  $r_{O_2} = \frac{V_{mO_2} [O_2]}{K_{mO_2} + (1 + [CO_2]/K_{iO_2})[O_2]} e^{(\frac{-E_{O_2}}{R} \cdot (\frac{1}{T_s} - \frac{1}{T_{ref}}))}$  (9)

159  $r_{CO_2} = \frac{V_{mCO_2} [O_2]}{K_{mCO_2} + (1 + [CO_2]/K_{iCO_2})[O_2]} e^{(\frac{-E_{CO_2}}{R} \cdot (\frac{1}{T_s} - \frac{1}{T_{ref}}))}$  (10)

160 The parameters used in calculation of  $r_{O_2}$ ,  $r_{CO_2}$  are given in Table 1. The rate of O<sub>2</sub>  
161 consumption and rate of CO<sub>2</sub> production are not equal thus average of these values is used to  
162 estimate the heat of respiration ( $Q_r$ ). This energy is used for the basic functions of cell but  
163 also a large component is used in evaporative water vapour from the surface of the  
164 commodity. The heat of respiration can be calculated from following equation (Rennie and  
165 Tavoularis, 2009).

166  $Q_r = \frac{2816}{6} \times \frac{r_{O_2} + r_{CO_2}}{2} \times \alpha \times W_s$  (11)

167 The chemical reaction indicates for every 6 moles of CO<sub>2</sub> produced, 2816 kJ heat is  
168 generated.  $\alpha$  is conversion factor of respiration energy dissipated as heat (ranging between  
169 0.8 to 1.0) (Song et al., 2002). In this work it is assumed that all the respiration heat produced  
170 is dissipated as heat thus  $\alpha = 1.0$ .

### 171 ***Permeability***

172 Film permeability is governed by the number and size of the film's perforations. The  
173 theoretical model is derived from the assumption that low molecular weight mass exchange at  
174 steady state conditions is given by two parallel mass fluxes-one related to permeation through  
175 the matrix Eq. (12)

$$176 P_i = P_{i \text{ ref}} + \frac{\pi R_h^2 \times D_{i, \text{air}}}{(L_f + R_h)} \times N_h \quad (12)$$

177 Where,  $P_i$  is the permeability of the film to ( $i=O_2$ , CO<sub>2</sub> and H<sub>2</sub>O),  $P_{i \text{ ref}}$  is the reference value  
178 of permeability of film to ( $i=O_2$ , CO<sub>2</sub> and H<sub>2</sub>O) at reference temperature,  $R_h$  is the radius of  
179 the perforation (m),  $D_{i, \text{air}}$  is diffusivity of ( $i=O_2$ , CO<sub>2</sub> and H<sub>2</sub>O) in air ( $m^2 \text{sec}^{-1}$ ),  $N_h$  is  
180 number of perforations.

### 181 **2.3.2. Transpiration**

182 Transpiration is an important physiological process which has an adverse effect on mushroom  
183 quality, influencing weight loss, appearance and texture. The factor which contributes to  
184 transpiration is the vapour pressure deficit VPD (Pa) Eq. (13), between the produce surface  
185 and the surrounding atmosphere (Xanthopoulos et al., 2012). VPD is the function of the  
186 difference in the amount of moisture in the air and the amount of moisture air can hold when  
187 it is saturated.

$$188 \text{VPD} = (a_w - \text{RH})p_s \quad (13)$$

189 In the above equation water activity ( $a_w \sim 1$ ) of the fresh produce is assumed and RH is  
190 relative humidity of the atmosphere surrounding the product.

191 Transpiration sets in when water vapour pressure at the surface of the commodity exceeds the  
 192 water vapour pressure of the headspace in the package. Water vapour flux ( $m_w$ ) is expressed  
 193 as the product of the transpiration coefficient and water vapour pressure deficit as Eq. (14)  
 194 (Becker et al., 1996; Xanthopoulos et al., 2012).

$$195 \quad m_w = VPD \times K_t \quad (14)$$

196 The transpiration rate ( $t_r$ ) is product of the water vapour flux ( $m_w$ ) and the surface area of  
 197 the commodity( $A_c$ ) Eq. (20)

$$198 \quad t_r = m_w A_c \quad (15)$$

$$199 \quad K_t = \frac{1}{\left(\frac{1}{K_s} + \frac{1}{K_a}\right)} \quad (16)$$

200 Here,  $K_t$  is the transpiration coefficient ( $\text{kg m}^{-2}\text{s}^{-1}\text{Pa}^{-1}$ ) which is constant for the specific  
 201 commodity,  $K_s$  ( $\text{kg m}^{-2}\text{s}^{-1}\text{Pa}^{-1}$ ) is the skin mass transfer coefficient obtained from literature  
 202 (Becker et al., 1996),  $K_a$  ( $\text{kg m}^{-2}\text{s}^{-1}\text{Pa}^{-1}$ ) is the air film mass transfer coefficient calculated  
 203 from equation 23 using the Sherwood-Reynolds-Schmidt correlations (Becker et al., 1996).

204 The saturated water vapour pressure ( $p_s$ ) is calculated from the following equation at the  
 205 surrounding air temperature( $T_s$ );

$$206 \quad p_s = 0.041081186T_s^3 - 32.43188T_s^2 + 8567.5269T_s - 757070.1 \quad (17)$$

207 For transpiration to take place energy is required to evaporate water from surface of the  
 208 produce which in turn cools the product. It is assumed that all the energy required for  
 209 transpiration is provided by the heat of respiration.

$$210 \quad Q_{tr} = \lambda t_r \quad (18)$$

### 211 **2.3.3. Condensation**

212 Due to near saturation conditions in the package and non-uniform temperature, condensation  
 213 can occur on surface of the produce, the package film and walls. It is assumed that the water  
 214 condensed on the surface of the produce does not penetrate its skin. The rate of condensation

215 on the surface of commodity  $M_{con}$  (kg sec<sup>-1</sup>) was calculated using Eq. (19) (Jalali et al., 2017;  
 216 Rennie and Tavoularis, 2009)

$$217 \quad M_{con} = \begin{cases} K_a(p_i - p_c)\delta A_c, & \text{if } (p_i > p_c) \\ 0 & \text{otherwise} \end{cases} \quad (19)$$

218 Where,  $A_c$  can be calculated as following assuming an equivalent spherical shape (Mahajan  
 219 et al., 2008).

$$220 \quad A_c = d \times W_s^b \quad (20)$$

221 The rate of condensation on the walls and film of package  $M_{wcon}$  can be calculated similarly  
 222 using the air film mass transfer coefficient ( $K_a$ ). Where  $A_w$  is inside surface area of the  
 223 package.

$$224 \quad M_{wcon} = \begin{cases} K_a(p_i - p_s)\delta A_w, & \text{if } (p_i > p_s) \\ 0 & \text{otherwise} \end{cases} \quad (21)$$

225 And rate of heat release due to condensation raises the temperature of air surrounding fresh  
 226 produce and determined using;

$$227 \quad Q_{con} = \lambda \times (M_{con} + M_{wcon}) \quad (22)$$

228 Where,  $K_a$  is air film mass transfer coefficient. The Sherwood-Reynolds-Schmidt  
 229 correlation is used to estimate the value of  $K_a$ .

$$230 \quad K_a = 2 \times D_{H_2O} \times \frac{M_{H_2O}}{d_c \times R \times T_s} \quad (23)$$

231 The latent heat of vaporisation  $\lambda$  (J kg<sup>-1</sup>) is estimated using;

$$232 \quad \lambda = (3151.37 + (1.805 T_s) - (4.186 T_s)) \times 1000 \quad (24)$$

233 The convective heat transfer coefficient ( $h_p$ ) is estimated by using the natural convection of  
 234 air (Song et al., 2002).

$$235 \quad h_p = \frac{0.59A_{p1}\left(\frac{T_i - T_o}{D_1}\right)^{0.25}}{A_p} + \frac{1.32A_{p2}\left(\frac{T_i - T_o}{D_2}\right)^{0.25}}{A_p} + \frac{1.42A_{p3}\left(\frac{T_i - T_o}{D_3}\right)^{0.25}}{A_p} \quad (25)$$

236

237 **2.4. Quality**

238 The quality of fresh produce is determined by the overall evaluation of various characteristics  
239 of the individual product. Perception of quality is subjective and depends largely on  
240 qualitative factors. To be able to predict the development of these quality characteristics as a  
241 function of storage time is highly desirable in order to support optimisation. The quality of  
242 fresh produce is generally determined by the overall characteristics (appearance, texture,  
243 flavour and nutritive value) of fresh produce (ElMasry et al., 2007).

244 **2.4.1. Colour in mushrooms**

245 Consumers consider the appearance of fresh produce into consideration as a primary  
246 criterion, with colour a key factor. Changes in colour occur due to various biochemical  
247 processes taking place in the produce over time. Browning of mushroom reduces the quality  
248 and is a limiting factor for its shelf life (Aguirre et al., 2008).

249 One of the major roles in modelling the quality in supply chain is the dynamics of quality  
250 degradation. Quality degradation of produce is dependent on storage time (t), temperature,  
251 and various constants such as the activation energy and gas constant.

252 
$$\frac{dq}{dt} = kq^n \quad (26)$$

253 Where, q is the quality parameter and k is rate of degradation depending on environmental  
254 conditions like temperature, n is the power factor is the order of reaction (n will have value 0  
255 or 1, zero order or first order reactions) leading to linear or exponential quality decay (Aiello  
256 et al., 2012; Rong et al., 2011).

257 A linear mixed effect model is used to model the effect of temperature and relative humidity  
258 on the apparent first order rate constant of the L value of mushroom caps. The kinetic  
259 dependence with time is studied using eq. 26.

$$k_L = (8.283477 \times 10^{-5}T_s) + (-7.181884 \times 10^{-4}RH) + (-1.258058 \times \quad (27)$$

$$10^{-5}T_s RH) + (-2.278137 \times 10^{-5}T_s^2) + (7.816388 \times 10^{-5}RH^2)$$

260 The mixed effect model estimated batch-to-batch and inside-batch variability components  
261 that are integrated in Table 2.

#### 262 **2.4.2. Weight loss**

263 Transpiration of water vapour from the surface of produce is one of the major contributor to  
264 weight loss observed in fresh produce. Carbon loss through gas exchange also contributes to  
265 weight loss in fresh produce as they continue respiring throughout storage. Here, we have  
266 assumed the weight loss ( $w$ ) to be equal to the amount of water permeated from the film  
267 ( $m_{pr}$ ) and carbon loss during respiration.

$$268 \frac{dw}{dt} = m_{pr} + r_{CO_2} W_s M_C \quad (28)$$

#### 269 *Stochastic Simulation and Sensitivity Analysis*

270 On the basis of the mathematical models developed in section 2, stochastic simulations were  
271 developed to analyse the effects of biological and cold chain variability on the quality  
272 characteristics of mushroom. The values of parameters used in our model to solve ordinary  
273 differential equations are shown in Table 1. All simulations were carried using the R 3.4.3 (R  
274 Development Core Team, 2008). The ODE model was integrated using the deSolve library  
275 (Soetaert et al., 2010) using the *lsoda* solver. All figures were produced using the ggplot2  
276 library (Wickham, 2009). Sensitivity analysis using a main and first order interactive effects  
277 model excluding time were analysed using a Lowry plot (McNally et al., 2011).

#### 278 **2.5. Cold chain variability**

279 The history of export of four international cold chains between Ireland and the United  
280 Kingdom, comprising temperature and relative humidity data including the production farm,  
281 the packaging house, international haulage, retail storage and arrival to the retail shop. The  
282 data was collected using temperature and relative humidity dataloggers (XSense®, BT9  
283 Intelligent Supply Chain Solutions, UK) with a logging frequency of 10 minutes and

284 comprised 4 export chains including at least 3 retail storage and arrival to 3 shops with 3  
285 replicates extending from 3 to 6 days depending on the different conditions.

286 In order to simulate the sales conditions cold chain data for the retail display scenario were  
287 added to this study. The study from Garvan (2007) was conducted throughout the summer of  
288 2007 including 85 premises spread through the 26 counties in the Republic of Ireland,  
289 including open and close refrigerated cabinets with a supermarket, a deli shop and a butcher  
290 outlet in each county.

## 291 **2.6. Validation Experiment**

292 Mushroom trays (250g of white, closed cup, 2.5 - 4 cm in diameter) packaged in  
293 microperforated polypropylene film (8 perforations per package) were supplied by Monaghan  
294 Mushrooms Ltd. Samples were stored in an environmental chamber under abuse condition  
295 (1/2h packaging at 8 °C followed by transportation at 4 °C up to 1 day, followed by retail  
296 storage including 4h at 20 °C, followed by 1 day at 8 °C, and finalised by retail shop 4h at 20  
297 °C 21h at 8 °C) and ideal condition in a refrigerator (at 3 °C) for a 7 days period

298 Mushroom tissues colour was measured using a Hunter colorimeter in the L\*, a\*, b\* scale  
299 (Colour Quest XE Hunter Lab, VA, USA). 30 measurements were taken per punnet. Three  
300 punnets were analysed per treatment and day. Moisture content was determined following the  
301 AOAC methods (32.1.02 and 32.1.03) (Lee, 1995). Photographic evidence of initial day and  
302 7 days storage can be inspected in the highlights section.

## 303 **3. Results**

### 304 **3.1. Validation of the mathematical model**

305 The model parameter estimates in Table 1 and 2 are used to compare the experimental and  
306 predicted results. The integrated mathematical model mentioned in section 2 is used to  
307 simulate the quality conditions during the distribution supply chain. The experimental data  
308 used for validation mimicked the results of an average and an abuse cold chain of recorded

309 cold chain information. The mushrooms were stored in commercial packaging at different  
310 temperatures simulating abuse conditions at (4<sup>0</sup>, 8<sup>0</sup>, and 20<sup>0</sup> C) and at ideal temperature of 3<sup>0</sup>  
311 C for 9 days. Mushroom colour was measured using the L value and the moisture content was  
312 measured using the AOAC methods. The mushrooms with L value >86 are classified as good  
313 quality and 80-85 as fair quality (González-Fandos et al., 2000). Those with L values less  
314 than 70 would be generally rejected by consumers (Kim et al., 2006). These L-value  
315 threshold values are used as indicators to calculate the losses during the supply chain.  
316 The mathematical model (section 2) was able to predict the changes in L values during  
317 storage. The grey ribbon in the Fig. 1 represents the uncertainty margins of 5% and 95%  
318 percentiles pertaining to the variable. It can be observed from figure that the experimental  
319 data with the variation falls in the prediction interval obtained from the simulation.  
320 Throughout the simulated cold chain, L value remains between the acceptable limits within  
321 82-95, even though the product was stored at different temperatures (4<sup>0</sup>, 8<sup>0</sup>, 20<sup>0</sup> C) Fig.1(a).  
322 When simulated at the ideal temperature of 3<sup>0</sup> C the change in L value was between 95 and  
323 89 Fig.1(c). The bias and accuracy factors of the L value prediction were and respectively.  
324 The change in moisture content of mushroom for the different temperatures (4<sup>0</sup>, 8<sup>0</sup>, 20<sup>0</sup> C) is  
325 shown in Fig.1(b). with the experimental data falling in the predicted interval. Similar results  
326 were obtained at the ideal temperature (3<sup>0</sup> C) (Fig. 1(d)). This shows the weight of mushroom  
327 is preserved in the packaging.

### 328 **3.2. Cold chain variability assessment**

329 The integrated mathematical model mentioned in section 2 is used to simulate the quality  
330 conditions during the distribution supply chain. The governing ordinary differential equations  
331 are used to simulate the changes in gas concentration Eq. (1 and 2), temperature Eq. (7) and  
332 relative humidity Eq. (4, 5) in the headspace of an ideally designed modified atmosphere  
333 pack and changes in quality are simulated against the supply chain conditions Fig. 2.



334 Changes in the respiration rate of mushroom causes changes in the concentration of O<sub>2</sub> and  
335 CO<sub>2</sub> in the headspace of package. CO<sub>2</sub> rises in the headspace of package, O<sub>2</sub> concentration  
336 decreases from 21% to 12% (Fig. 2(a)) and CO<sub>2</sub> concentration increases from 0.03% to  
337 <10% when simulated against the export cold chain profile (Fig. 2(b)). These results are in  
338 agreement with (Cliffe -Byrnes and O'Beirne, 2007)  
339 where O<sub>2</sub> concentration changes from 20 to 2 % when mushrooms are stored at 5 different  
340 temperatures (4, 8, 10, 13 and 16<sup>0</sup> C) representing abuse temperature. The relative humidity  
341 inside the package saturates within a few hours of storage. Similar results were obtained by  
342 (Rux et al., 2015) in mushrooms, (Song et al., 2002) for blueberry and (Fishman et al., 1996)  
343 for mango stored in MAP. Fig. (2(c)) shows the weight loss observed during the supply  
344 chain. The typical kinetic change of quality (L value) during the distribution supply chain is  
345 shown in Fig. 2(d). The variability decreases towards the end of storage. (Jiang et al., 2011)  
346 reported that the L value decreased to 81.8 and 78.1 after 8 and 12 days storage respectively  
347 at 4<sup>0</sup> C in MAP, after which the product passes the threshold for acceptable quality for  
348 *Agaricus bisporus*.

### 349 **Sources of variability**

350 The main sources of biological variability associated with mushroom are the Michaelis-  
351 Menten respiration parameters and the activation energy parameters associated with these  
352 constants (Table 1). For quality the biological variability is described by the initial colour  
353 values (L, a, b value), initial weight of the produce and the skin mass transfer coefficient  
354 (Table 1).

### 355 **3.3. Product variability assessment**

356 The mathematical model is used to simulate and predict the effect of input product parameter  
357 uncertainty on the quality of mushroom. The time domain for simulation is 7 days at (3<sup>0</sup>, 7<sup>0</sup>,  
358 15<sup>0</sup>C). The optimal storage guide for mushroom storage to maximise its quality and shelf life

359 is 1-3<sup>0</sup> C and as high RH as possible (Aguirre et al., 2008). The effect of product parameter  
360 variation on the CO<sub>2</sub> concentration at different temperatures of storage is presented in Fig.  
361 3(a). The rate at which the propagation of the biological variation increases depends directly  
362 on temperature. The variation observed at 15<sup>0</sup> C is larger than observed in other cases. In the  
363 case of O<sub>2</sub> the variation increases with increase in temperature, with similar results observed  
364 for CO<sub>2</sub>. Anaerobic conditions are not observed at 3<sup>0</sup>C and 7<sup>0</sup>C as evident from Fig. 3(b).  
365 However, anaerobic conditions are observed at 15<sup>0</sup> C after 5 days.

366 Weight loss in mushrooms is mainly caused by transpiration of water from surface of  
367 mushroom and CO<sub>2</sub> loss through respiration Eq. (28). More weight loss is observed when  
368 mushrooms are stored at higher temperatures, which is due to the increase in transpiration  
369 and respiration rates Fig. 4(a). The effect of product variation on weight loss in mushroom  
370 was not found. The maximum weight loss of 2.47% was noted after 16 days MAP storage at  
371 4<sup>0</sup> C (Jiang et al., 2011). (Roy et al., 1995) reported weight loss of 3% (120 g) and 4.5% (50  
372 g) in packages after 9 days storage when stored at 12<sup>0</sup>C. The maximum variation due to  
373 product parameters is observed for the L value as evident from Fig. 4(b). With increase in  
374 temperature the variation increases and the acceptability threshold is thus crossed at 15<sup>0</sup> C in  
375 both cases of weight loss and L value. Based on these results a lower temperature during the  
376 supply chain distribution is preferred as the variation associated with it is less, to retain the  
377 quality of mushroom and to reduce the losses during distribution chain.

#### 378 **3.4. Comparing the importance of variability components on quality kinetics of** 379 **Mushroom under distribution conditions**

380 Relative frequency is plotted against the time of storage for the different characteristics of the  
381 produce to compare the effect of variability due different sources (Table 2). The  
382 concentrations of gases (O<sub>2</sub> and CO<sub>2</sub>) in the headspace of the package are influenced by the  
383 product variability parameters as evident from Fig. 5(a) and (b). For the L-value the main

384 influence observed is from the product parameters Fig. 5(c). This result is in agreement with  
385 the general practice in postharvest technology of mushroom which includes grading and  
386 sorting of produce before packing to reduce variability on how product is affected by  
387 storage/distribution supply chain. To obtain the final product with the highest L value, the  
388 initial value of the product should be higher. In the case of weight loss in mushrooms it is  
389 influenced by the cold chain parameters Fig. 5(d). The temperature and relative humidity  
390 during storage will influence the rate of moisture loss during the distribution supply chain.  
391 Relatively small weight loss of 3-6 % in fruits and vegetables is sufficient to cause wilting,  
392 shrivelling and dryness. In addition to this it causes significant economic losses (Nunes et al.,  
393 2009).

### 394 **3.5. Sensitivity analysis**

395 Uncertainty analysis usually accompanies sensitivity analysis which quantifies the  
396 contribution of each input parameter to the output parameters (Guillard et al., 2012).  
397 Sensitivity analysis is performed to study the results of variation and how it can be  
398 apportioned qualitatively or quantitatively to different sources of variation in the model input  
399 (Kader and Saltveit, 2003).

400 The result of sensitivity analysis for L value shows that initial L value as 100% contributor  
401 towards the variability Fig. 5(a). The results of sensitivity analysis of CO<sub>2</sub> indicate the  
402 Michaelis-Menten respiration rate constants to have the highest impact on the concentration  
403 of CO<sub>2</sub> in the headspace (90%). The results of sensitivity analysis of weight loss are  
404 presented in the Fig. 5(b). The activation energy rate constant which are dependent on  
405 temperature have highest impact on the weight loss of mushroom in supply chain. Along with  
406 respiration rate parameters it contributes to 90% variability. Some variability was observed  
407 due to the interactions between the parameters like skin mass transfer coefficient and initial

408 weight of mushroom. To tackle the loss of weight of mushroom, the cold chain variations  
409 (Temperature and Relative humidity) should be managed throughout supply chain.

#### 410 **4. Conclusions**

411 A mathematical model is developed to predict the change observed in the quality of  
412 mushroom packed in modified atmosphere packaging during storage. The model integrates  
413 mass transfer processes including; transpiration, transport of gases (O<sub>2</sub>, CO<sub>2</sub>) and heat  
414 transfer process like respiration heat, convection through produce into surroundings,  
415 transpiration heat and heat of condensation. The comparison of effect of biological  
416 parameters (respiration rate parameters and initial quality) and the cold chain parameters  
417 (relative humidity and temperature) on the quality of mushroom was observed. To quantify  
418 the effect on the biological parameters, sensitivity analysis was performed which explained  
419 the effect of the main parameters and the interactions between the parameters. In terms of  
420 colour change of the mushroom, the initial L value variation showed to be the most  
421 contributory factor to variations during distribution and cold chain, while the weight loss  
422 depended on a larger number of process and product parameters.

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429

<b>Nomenclature</b>
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$a_w$	Water activity of fresh produce	$P_i$	Film permeability to species (i=O <sub>2</sub> , CO <sub>2</sub> , H <sub>2</sub> O) (ml m m <sup>-2</sup> h <sup>-1</sup> atm <sup>-1</sup> )
$A_c$	Surface area of produce (m <sup>2</sup> )	$P_{i\ ref}$	Reference Permeability of film to i=O <sub>2</sub> , CO <sub>2</sub> , H <sub>2</sub> O (ml m m <sup>-2</sup> h <sup>-1</sup> atm <sup>-1</sup> )
$A_{p1}$	Surface area of packaging film (m <sup>2</sup> ) ( $D_1 \times D_2$ )	$Q_{con}$	Condensation heat released due to commodity (Js <sup>-1</sup> )
$A_{p2}$	Surface area of bottom of package (m <sup>2</sup> ) ( $D_1 \times D_2$ )	$Q_r$	Heat of respiration (J h <sup>-1</sup> )
$A_{p3}$	Surface area of walls of package (m <sup>2</sup> )	$Q_{tr}$	Evaporative heat transfer due to transpiration (Js <sup>-1</sup> )
$A_p$	Total surface area of package (m <sup>2</sup> )	$r_{CO_2}$	CO <sub>2</sub> production rate (mol kg <sup>-1</sup> s <sup>-1</sup> )
$C_a$	Humid heat of air (J kg <sup>-1</sup> K <sup>-1</sup> )	$r_{O_2}$	O <sub>2</sub> consumption rate (mol kg <sup>-1</sup> s <sup>-1</sup> )
$C_s$	Specific heat of produce (J kg <sup>-1</sup> K <sup>-1</sup> )	$R$	Gas constant (8.314 J mol <sup>-1</sup> K <sup>-1</sup> )
$E_{O_2,CO_2}$	Activation energy of rate constant (Jmol <sup>-1</sup> )	$R_h$	Radius of perforation (m)
$d_c$	Equivalent diameter of produce (cm)	RH	Relative humidity inside package (%)
$d_H$	Diameter of perforation (mm)	RH <sub>o</sub>	Relative humidity outside package (%)
$D_1 \times D_2 \times D_3$	Dimensions of package (cm)	t	Time (s)
$D_{i,air}$	Diffusion coefficient of i=O <sub>2</sub> , CO <sub>2</sub> , H <sub>2</sub> O in air (m <sup>2</sup> s <sup>-1</sup> )	$t_r$	Transpiration rate (kg m <sup>-2</sup> h <sup>-1</sup> )
$h_p$	Convective heat transfer coefficient on produce surface (Jh <sup>-1</sup> m <sup>-2</sup> K <sup>-1</sup> )	$T_i$	Temperature inside package (K)
$K_a$	Air film mass transfer coefficient (kg m <sup>-2</sup> s <sup>-1</sup> Pa <sup>-1</sup> )	$T_o$	Temperature outside package (K)
$K_s$	Skin mass transfer coefficient (kg m <sup>-2</sup> s <sup>-1</sup> Pa <sup>-1</sup> )	$T_s$	Temperature of surface produce (K)
$K_t$	Transpiration coefficient (kg m <sup>-2</sup> s <sup>-1</sup> Pa <sup>-1</sup> )	$T_{ref}$	Produce reference temperature (K)
$K_{mO_2}$	Michealis constant in O <sub>2</sub> consumption (% O <sub>2</sub> )	$V_b$	Bulk volume of produce (m <sup>3</sup> )
$K_{mCO_2}$	Michealis constant in CO <sub>2</sub> evolution (% O <sub>2</sub> )	$V_f$	Free volume in headspace (ml) (
$K_{iO_2}$	Inhibition constant in O <sub>2</sub> consumption (% CO <sub>2</sub> )	$V_{mO_2}$	Maximum O <sub>2</sub> consumption rate (ml kg <sup>-1</sup> h <sup>-1</sup> )
$K_{iCO_2}$	Inhibition constant in CO <sub>2</sub> evolution (% CO <sub>2</sub> )	$V_{mCO_2}$	Maximum CO <sub>2</sub> evolution rate (ml kg <sup>-1</sup> h <sup>-1</sup> )
$L_f$	Thickness of packaging film (m)	VPD	Vapour pressure deficit (Pa)
$m_{pr}$	Rate of water permeation through film (kg sec <sup>-1</sup> )	$W_a$	Weight of dry air (kg)
$M_{con}$	Condensation rate on commodity (kgs <sup>-1</sup> )	$W_s$	Weight of produce (kg)

$M_{wcon}$	Condensation rate on package walls (kgs <sup>-1</sup> )	$[CO_2]_i$	CO <sub>2</sub> concentration inside package (%)
$M_i$	Molar mass of species (i= O <sub>2</sub> , CO <sub>2</sub> , H <sub>2</sub> O, C )(kg mol <sup>-1</sup> )	$[CO_2]_o$	CO <sub>2</sub> concentration outside package (%)
$N_h$	Number of perforations	$[O_2]_i$	O <sub>2</sub> concentration inside package (%)
$p_i$	Partial vapour pressure inside package (Pa)	$[O_2]_o$	O <sub>2</sub> concentration outside package (%)
$p_c$	Partial vapour pressure at commodity surface (Pa)	Greeks	
$p_o$	Partial vapour pressure outside package (Pa)	$\alpha$	Heat conversion factor
$p_s$	Saturated vapour pressure (Pa)	$\epsilon$	Porosity
$P_{atm}$	Atmospheric pressure =101325 Pa	$\lambda$	Latent heat of vaporization (J kg <sup>-1</sup> )
		$\rho_b$	Bulk density of produce (kg m <sup>-3</sup> )

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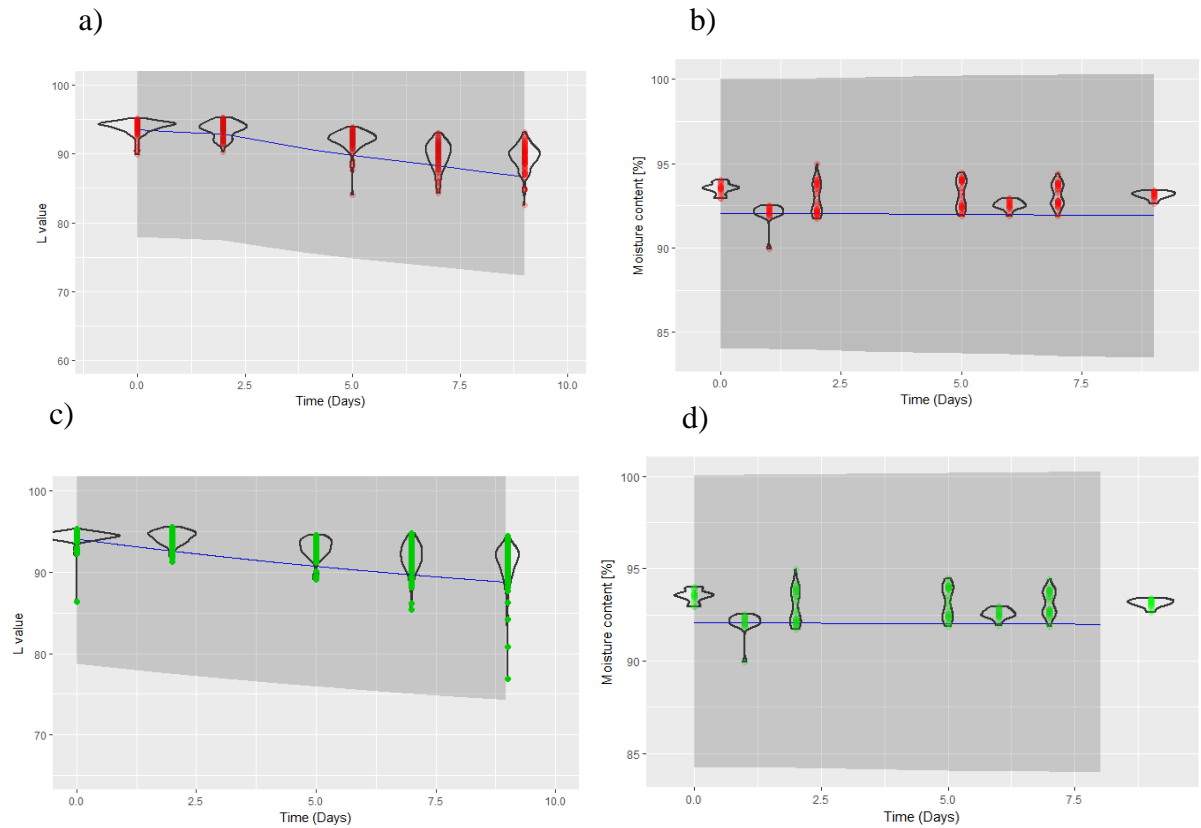


**Table 1 Properties of package, film and produce** (Borchert et al., 2014; Iqbal et al., 2009; Lu et al., 2013; Mahajan et al., 2008; Rux et al., 2015; Simón et al., 2010)

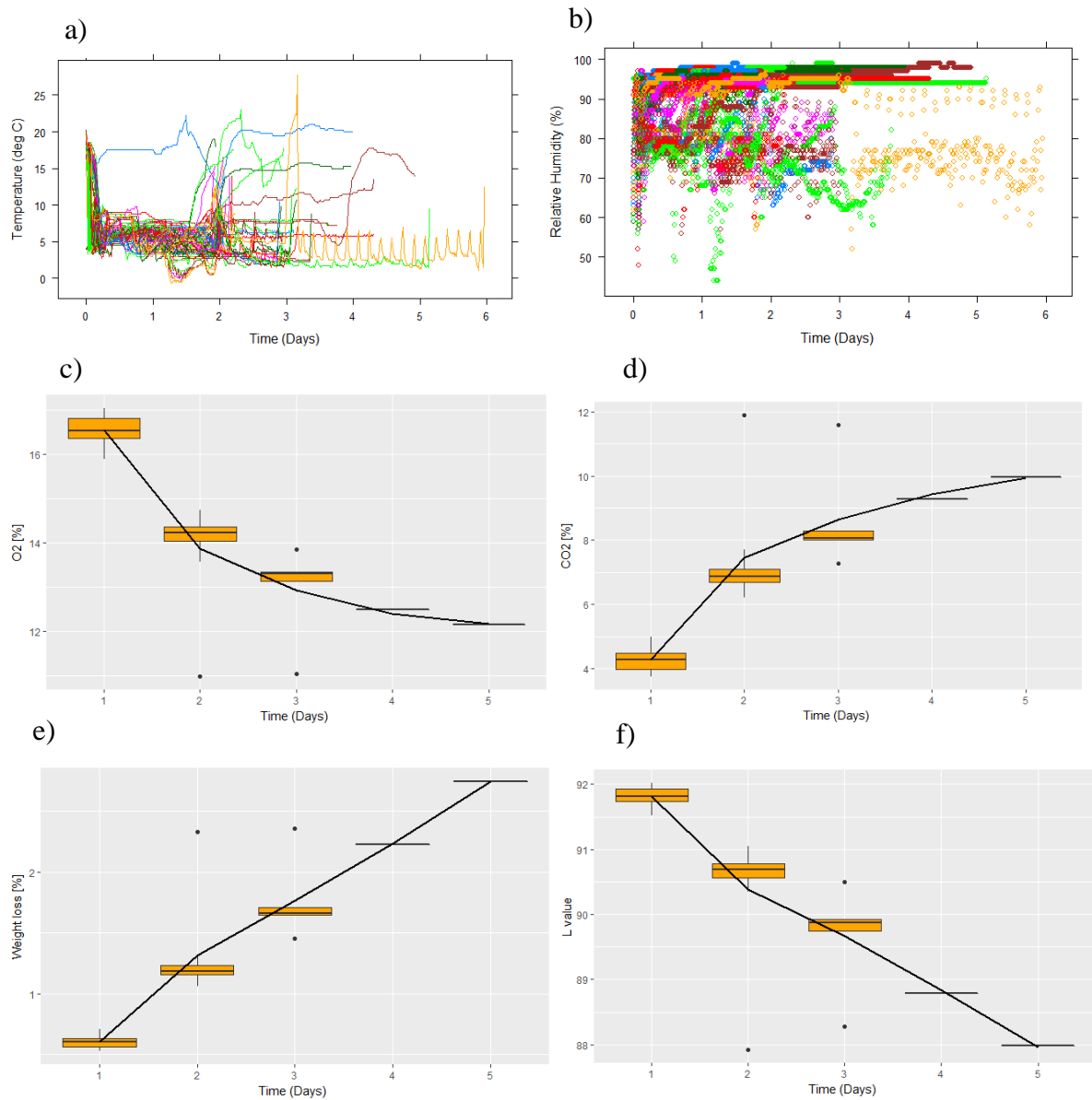
<b>Parameter</b>	<b>Value</b>
$a_w$	0.99
$\rho_b$ (kg m <sup>-3</sup> )	561
$C_s$ (J kg <sup>-1</sup> K <sup>-1</sup> )	3990
$D_1 \times D_2 \times D_3$ (cm <sup>3</sup> )	11.9 × 16 × 5.8
$d_c$ (cm)	4
$d_H$ (micron)	150
$N_h$	8
$L_f$ (m)	33.9 × 10 <sup>-6</sup>
$M_{O_2}$	0.032
$M_{CO_2}$	0.044
$M_{H_2O}$	0.018
$\epsilon$	0.2595
$W_s$ (kg)	0.250
$P_{CO_2ref}$ (mL.m.m <sup>-2</sup> h <sup>-1</sup> )	16.12 × 10 <sup>-13</sup>
$P_{O_2ref}$ (mL.m.m <sup>-2</sup> h <sup>-1</sup> )	5.66 × 10 <sup>-13</sup>
$P_{H_2Oref}$ (mL.m.m <sup>-2</sup> h <sup>-1</sup> )	4.32 × 10 <sup>-14</sup>

**Table 2 Parameter estimate and the standard error associated** (Aguirre et al., 2008; Iqbal et al., 2009b; Mahajan et al., 2008). L value<sub>i</sub>, a-value<sub>i</sub>, b-value<sub>i</sub> initial values, ( )<sub>b</sub> standard deviation associated with batch variability ( )<sub>s</sub> standard deviation associated with sample variability.

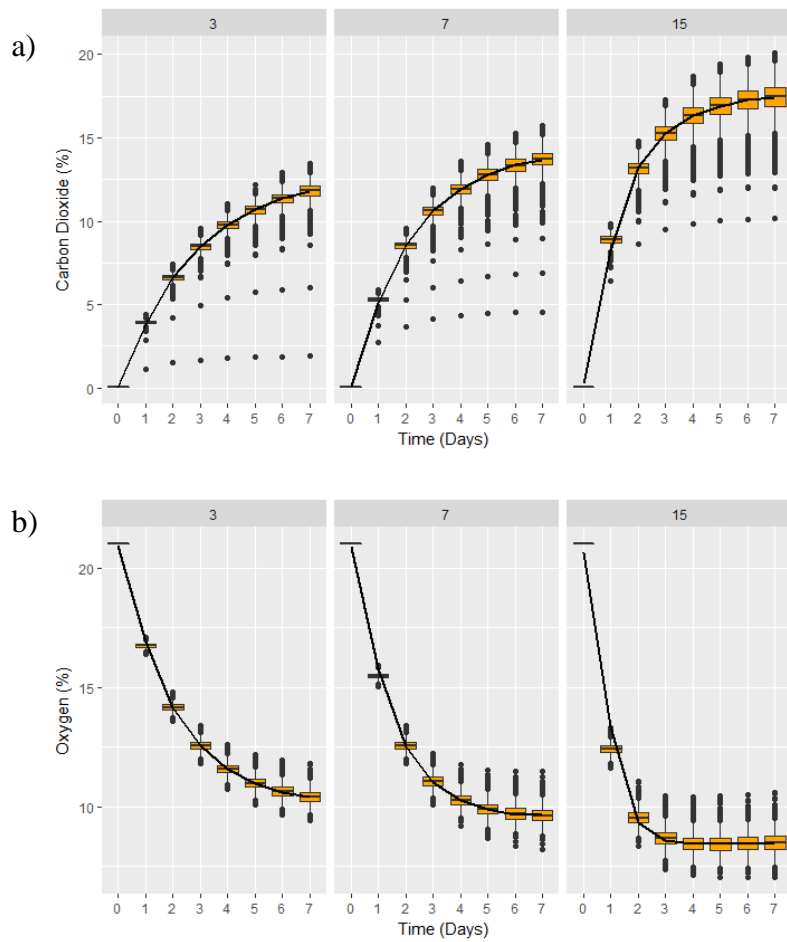
<b>Parameter</b>	<b>Value</b>
$V_{mO_2}$	63.64±1.13 (mL kg <sup>-1</sup> h <sup>-1</sup> )
$E_{O_2}$	54.38±1.07 (kJ mol <sup>-1</sup> )
$K_{mO_2}$	4.09±0.285 (%)
$K_{iO_2}$	38.60±5.03 (%)
$V_{mCO_2}$	54.68±1.19 (mL kg <sup>-1</sup> h <sup>-1</sup> )
$E_{CO_2}$	56.04±1.44 (kJ mol <sup>-1</sup> )
$K_{mCO_2}$	3.18±0.296 (%)
$K_{iCO_2}$	57.90±13.53 (%)
L-value <sub>i</sub>	93 (0.008) <sub>b</sub> (0.007) <sub>s</sub>
a-value <sub>i</sub>	0.77 (0.9) <sub>b</sub> (-) <sub>s</sub>
b-value <sub>i</sub>	10.6 (1.57) <sub>b</sub> (2.4) <sub>s</sub>
$K_s$	8.5 x10 <sup>-3</sup> (cm h <sup>-1</sup> )



**Fig. 1. Comparison of model predictions with the experimental data (points) at different temperature conditions (4, 8, 20<sup>0</sup> C) (red points) and at ideal temperature (3<sup>0</sup>C) (green points) a) Change of L value over time and b) Moisture content (% w/w) of mushroom at (4, 8, 20<sup>0</sup> C), c) Change of L value over time and d) Moisture content (% w/w) of mushroom at (3<sup>0</sup>C). The black line contour in each of the experimental levels indicates the distribution of the experimental data as a violin plot.**

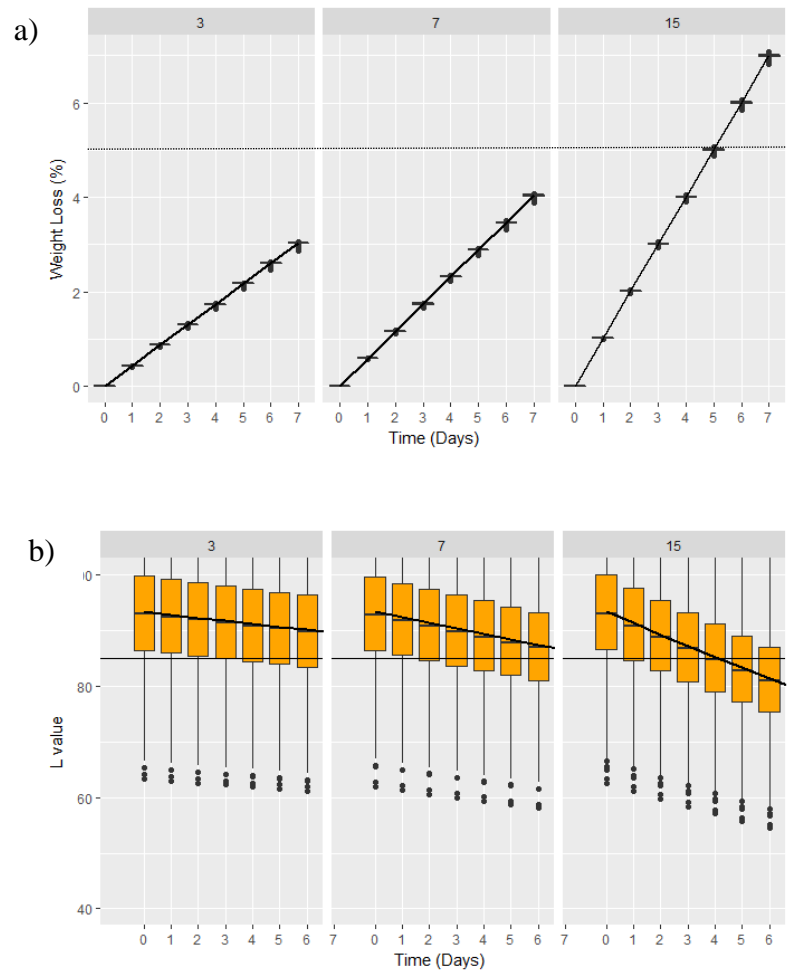


**Fig. 2. Prediction of the effect of a) temperature and b) relative humidity cold chain variation on c) O<sub>2</sub>, d) CO<sub>2</sub> in the headspace of package, e) weight loss and f) change in L value during supply chain.**

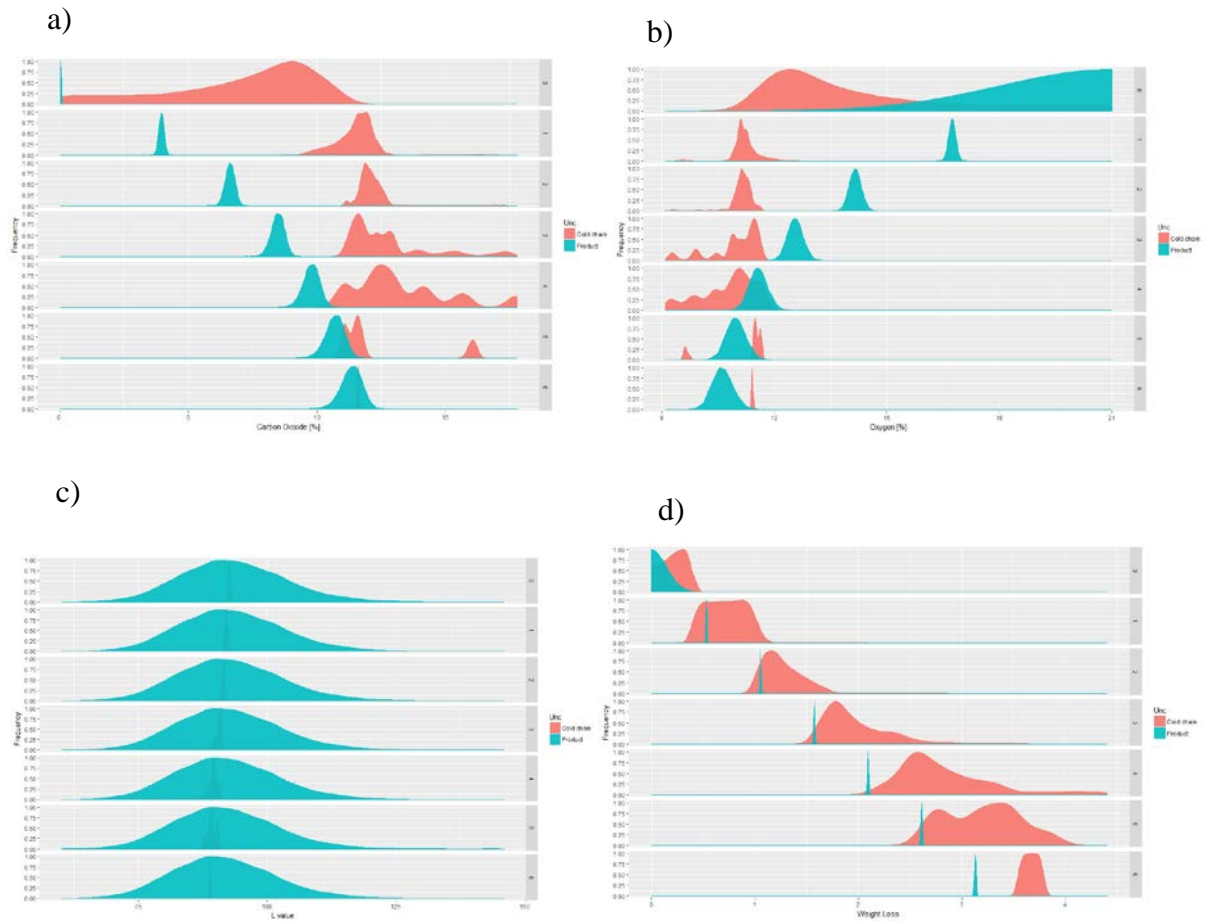


**Fig. 3. Propagation of effect of product parameters on the a) carbon dioxide concentration (b) oxygen concentration of mushroom tray packaging stored at different temperature (3, 7, 15 °C) in cold chain.**

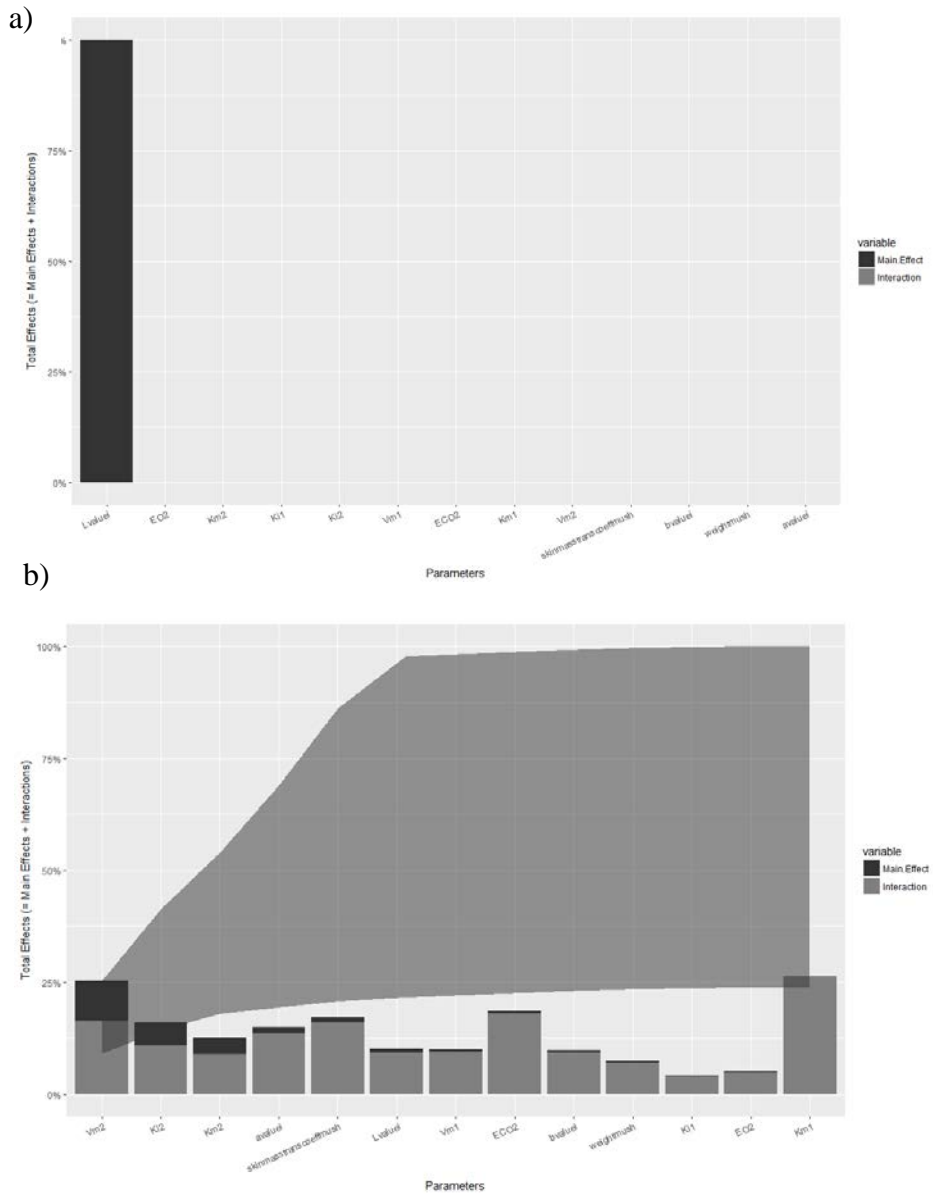




**Fig. 4. Propagation of effect of product parameters on the a) weight loss (b) L value of tray packed mushroom stored at different temperature (3, 7, 15 °C) in cold chain.**



**Fig. 5. Comparison of the effect of cold chain parameters and product parameters on the a) CO<sub>2</sub>, b) O<sub>2</sub> concentration in the headspace of package, c) L value and d) weight loss observed during distribution supply chain. Each subplot provides a kernel density distribution estimate arising from either the cold chain (pink) or product variability (blue) from day 0 (initial conditions) to day 6 of storage indicated in the right hand facet.**



**Fig. 6. Lowry plot for sensitivity analysis (The total effect of main parameter given in black and any first order interaction with other parameters is grey given as a proportion of variance. The ribbon represents variance due to parameter interactions, the cumulative sum of main effect is lower line and the sum of total effect is upper line) (a) L value and (b) weight loss.**