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Predicting Quality Attributes and Waste of Strawberry Packed Under Modified Atmosphere Throughout the Cold Chain

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1 **Predicting quality attributes and waste of strawberry packed under modified**
2 **atmosphere throughout the cold chain**

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10 **Abstract**

11 Modified Atmosphere Packaging (MAP) is used commercially to extend the shelf life of
12 strawberries. The attainment of desired gas (O₂, CO₂) concentrations inside MAP relies
13 on the product respiration and the mass transfer through packaging and will affect the
14 quality. The objective of this work is to build a mathematical model for strawberries to
15 assess the effect of the uncertainties on headspace gas concentration and quality: 1) cold
16 chain related temperature and relative humidity variations and 2) variability associated to
17 product respiration and quality based on literature. Weight loss was more influenced by
18 the cold chain storage conditions (temperature and RH) whereas spoilage had similar
19 influence of cold chain conditions and product parameters. Waste generated in the cold
20 chain was estimated from industrial standard weight loss and spoilage thresholds. A
21 sensitivity analysis of the stochastic MAP model showed the influence of input
22 parameters on the quality pointing to interventions associated to a reduction of the
23 respiration rate (e.g. modification of packaging) and reduction of water transfer (e.g.
24 coating) may prove more successful than other interventions to which the waste
25 generation of this product is not so sensitive to. As a conclusion this work presents a

26 toolbox to interpret cold chain data: 1) develop mathematical models to predict fate of
27 quality 2) simulate cold chain conditions allowing for uncertainty 3) estimate the waste
28 generation kinetics based in quality criteria and thresholds 4) perform a sensitivity
29 analysis to identify most sensitive technological parameters 5) identify interventions that
30 will affect those technological parameters.

31 **Keywords:** mathematical modelling; coating, variability; sensitivity analysis; strawberry

32 **1. Introduction**

33 Strawberries are highly perishable in nature with high metabolic rate and thus have short
34 shelf life. The major limiting factor of the quality of strawberries is spoilage due to
35 *Botrytis* infection. The tissue of strawberry deteriorates through natural senescence during
36 the food distribution chain and *Botrytis* develops due to tissue softening because of over
37 ripening (Hertog et al., 1999). The most effective intervention to extend the shelf life is
38 to use low temperature storage (Sanz et al., 2000). Packaging is another important
39 technique to extend the shelf life of perishable fruit to facilitate longer transportation
40 distribution (Caner et al., 2008). The storage quality can be further improved by using
41 Modified atmosphere packaging (MAP) and altering the concentration of gases
42 surrounding the fresh strawberry (Geysen et al., 2005; Zhang et al., 2003).

43 MAP has been used to increase and preserve the shelf-life of produce, while also
44 responding to the emerging consumer demand for convenience and quality (Oliveira *et*
45 *al.*, 2012b). Design of optimal Modified Atmosphere Packaging for specific produce
46 depends on the characteristics of produce, permeability of packaging film and dependence
47 on external factors such as temperature and relative humidity (Zagory e Kader, 1988).
48 Apart from extending the shelf life of strawberries it maintain the quality characteristics
49 firmness, prevents weight loss and microbial spoilage (Caner et al., 2008; Larsen and
50 Watkins, 1995; Pelayo et al., 2003).

51 **Sources of uncertainty in postharvest distribution of strawberries**

52 Managing uniform quality of produce is a tedious task because of many sources of
53 variability, inherent biological variation and fluctuation in storage conditions (Duret et
54 al., 2015). Postharvest management aims at controlling the variation as much as possible
55 by sorting and grading product at different stages of postharvest chain (Hertog et al.,
56 2009a). Identifying and quantifying different sources of variance in the experimental data
57 and assigning them to uncertainties in parameter value and error provides better
58 interpretation of postharvest behaviour (Aguirre, 2008; Hertog et al., 2007a). Biological
59 variation has been previously studied by including this variation in the quality change
60 model, estimating the initial variation (“harvest age”) and using it to assess the effect
61 throughout the postharvest chain (Hertog et al., 2009b). Over the last decade models
62 explaining biological variation in fresh produce have been developed (Duret et al., 2015;
63 Gwanpua et al., 2014; Hertog et al., 2007b, 2004).

64 In a MAP gas exchange kinetic model the uncertainty can also be estimated at the
65 respiration models of the strawberries. Michaelis-Menten inhibition constants for O₂
66 consumption (Km_{O_2}) and constant for fermentative CO₂ production ($Kmc_{O_2(f)}$), the
67 reference rate constant of maximum oxygen consumption (Vm_{O_2}) and maximum carbon
68 dioxide production ($Vm_{CO_2(f)}$) and the activation energy rate that have been
69 experimentally assessed will have uncertainty, conventionally in the form of a standard
70 error, associated to it (Hertog et al., 1999).

71 When describing the kinetics of weight loss in a packaged produce, the fruit skin mass
72 transfer coefficient (K_s) is one of the main source of product variation due to structural
73 variation in skin of individual fresh produce along with the initial spoilage of batch (N_0)
74 (Hertog et al., 1999). The statistical values of these parameters are presented in Table 2.

75 The objective of this study is to predict the quality of strawberry in supply cold chain. To

76 study the effect of cold chain variability and product variability on the quality of
77 strawberry which will help estimate the waste generated. Sensitivity analysis is then
78 performed to account for the effect of different parameters and design an intervention that
79 will reduce losses in supply chain.

80 **2. Materials and method**

81 **2.1. Model hypothesis**

- 82 1. CO₂ production is a combination of oxidative and fermentative production, the
83 oxidative consumption is proportional to the O₂ evolution and the fermentative
84 production follows the Michaelis-Menten equations.
- 85 2. The temperature of the surface of commodity (T_s) is equal to the temperature of
86 air surrounding the commodity (T_i).
- 87 3. The surface of the commodity is assumed to be perfectly saturated condition.
- 88 4. The metabolic energy released by produce, large part of it (80-100 %) is
89 dissipated as heat.
- 90 5. Condensation of water may occur in the product or the package when the free
91 volume air relative humidity reaches 100% using a saturated surface model.
- 92 6. The quality of strawberry is described as weight loss due to transpiration and by
93 *Botrytis* spoilage as modelled by (Hertog et al., 1999).

94 **2.2. Mathematical Model development**

95 The mathematical model takes into account the heat and mass transfer balances due to the
96 metabolic behaviour of strawberry and the transport phenomenon across package. The
97 assumptions used in the mathematical model and sub model to describe respiration-
98 transpiration of strawberry and gas transport across package (Table 1). The influence of
99 these on the quality of strawberry during distribution chain is estimated.

100 **2.2.1. Transpiration**

101 Transpiration is caused due to vapour pressure deficit VPD (Pa) between the produce
102 surface and the surrounding atmosphere (Xanthopoulos et al., 2012). VPD is the function
103 of difference in the amount of moisture in air and the amount of moisture air can hold
104 when it is saturated (Becker et al., 1996).

$$105 \quad VPD = (a_w - RH)p_s \quad (11)$$

106 It is assumed that water activity of strawberry is ($a_w \sim 0.99$).

107 Saturated water vapour pressure at the surface of commodity can be calculated using
108 following equation (Rennie and Tavoularis, 2009) based on saturated water vapour
109 pressure data from ASHRAE (1997).

$$110 \quad p_s = 0.041081186T_s^3 - 32.43188T_s^2 + 8567.5269T_s - 757070.1 \quad (12)$$

111 Transpiration occurs when water vapour pressure at the surface of commodity exceeds
112 the water vapour pressure of the headspace of package (Becker et al., 1996; Xanthopoulos
113 et al., 2012).

$$114 \quad m_w = VPD \times K_t \quad (13)$$

115 Transpiration rate ($\text{kg m}^{-2}\text{h}^{-1}$) is product of water vapour flux (m_w) and the surface area
116 of the commodity (A_c)

$$117 \quad t_r = m_w A_c \quad (14)$$

$$118 \quad K_t = \frac{1}{\left(\frac{1}{K_s} + \frac{1}{K_a}\right)} \quad (15)$$

119 Here, K_t is transpiration coefficient ($\text{kg m}^{-2}\text{s}^{-1}\text{Pa}^{-1}$) which is constant for the same
120 commodity, K_s ($\text{kg m}^{-2}\text{s}^{-1}\text{Pa}^{-1}$) is skin mass transfer coefficient obtained from literature,

121 K_a ($\text{kg m}^{-2}\text{s}^{-1}\text{Pa}^{-1}$) is air film mass transfer coefficient calculated using the Sherwood-
122 Reynolds-Schmidt correlations (Becker et al., 1996) .

$$123 \quad Sh = \frac{K_a d_c}{D_{H_2O,air}} \quad (16)$$

124 For convective mass transfer from commodity spherical in shape, (Becker et al., 1996)
125 recommended Sherwood-Reynolds-Schmidt correlation of the following form to be used.

$$126 \quad Sh = 2.0 + 0.552 Re^{0.53} Sc^{0.33} = \frac{K'_a d_c R T_s}{D_{H_2O,air} M_{H_2O}} \quad (17)$$

127 It is assumed, there is negligible flow around the commodity ($Re \approx 0$). Therefore, air
128 film mass transfer coefficient can be calculated as:

$$129 \quad K_a = 2 \times \frac{D_{H_2O-air} M_{H_2O}}{d_c R T_s} \quad (18)$$

130 *Transpiration Heat*

131 The process of transpiration requires energy for evaporation of moisture from surface of
132 produce, this process cools down the commodity. Evaporative heat transfer rate (Q_{tr}) is
133 a product of latent heat of vaporization (λ) and transpiration rate (t_r).

$$134 \quad Q_{tr} = \lambda t_r \quad (19)$$

135 **2.2.2. Relative humidity in headspace**

136 The concentration of water vapour inside the package is dependent on the rate of water
137 vapour transfer from the moisture sources to moisture sinks within the package. The main
138 moisture sources in the package is water transpired from the surface of fresh produce (t_r)
139 and the main source of moisture sink is permeation of water vapour through the film
140 (m_{pr}) (Becker et al., 1996).

141 The amount of water vapour in the headspace is calculated using humidity ratio which is
 142 the ratio of mass of water vapour in headspace to mass of dry air in the headspace of
 143 package (kg/kg).

$$144 \quad \frac{dHR}{dt} = \frac{t_r - m_{pr}}{W_a} \quad (20)$$

145 Relative humidity is calculated as ratio of humidity ratio inside the package (HR) to the
 146 humidity ratio of saturated water vapour (HR_{sat}) (Becker et al., 1996; Jalali et al., 2017;
 147 Song et al., 2002).

$$148 \quad HR_{sat} = \frac{0.62198P_s}{(P_{atm} - P_s)} \quad (21)$$

$$149 \quad RH = \frac{HR}{HR_{sat}} \quad (22)$$

150 **2.2.3. Condensation**

151 In perforation mediated packaging condensation rate is seldom modelled in MAP, due to
 152 near saturation conditions and non-uniform or fluctuating temperature within the
 153 package, condensation can occur on the commodity surface or inside of package film and
 154 walls. It is assumed that the water vapour condensed on the surface of commodity does
 155 not penetrate the skin of fresh produce. For condensation to take place the partial pressure
 156 of water vapour should be greater than the saturated water vapour pressure (Jalali et al.,
 157 2017; Joshi et al., 2018; Rennie and Tavoularis, 2009).

$$158 \quad M_{con} = \begin{cases} K_a (P_{H_2O} - P_c) \delta A_c, & \text{if } (P_{H_2O} > P_s) \\ 0 & \text{otherwise} \end{cases} \quad (23)$$

159 The corresponding rate of release of heat due to condensation on the surface of
 160 commodity is Q_{con} calculated as:

$$161 \quad Q_{con} = \lambda M_{con} \quad (24)$$

162 The rate of condensation on package wall (M_{wcon}) is calculated similarly using air film
163 mass transfer coefficient (K_a).

$$164 \quad M_{wcon} = \begin{cases} K_a(P_{H_2O} - P_s)\delta A_w, & \text{if } (P_{H_2O} > P_s) \\ 0 & \text{otherwise} \end{cases} \quad (25)$$

165 The heat released during condensation (Q_{wcon}) heats up gases in atmosphere near wall.

$$166 \quad Q_{wcon} = \frac{\lambda M_{wcon}}{A_w} \quad (26)$$

167 **2.2.4. Quality**

168 The quality of fresh produce is determined by the overall characteristics (appearance,
169 texture, flavour and nutritive value) of fresh produce (ElMasry et al., 2007). The
170 perception of quality is highly subjective and depends on consumer and number of
171 qualitative factors. Quality of fresh produce in general is often described using a chemical
172 kinetic model (Merts, 1996). The main attributes of quality in strawberries is weight loss
173 and spoilage.

174 **2.2.4.1. Weight loss**

175 The amount of water vapour transpired from the surface of fruit (t_r) and carbon loss due
176 to respiration accounts for the weight loss.

$$177 \quad \frac{dW_l}{dt} = t_r + M_c r_{CO_2} W_s \quad (27)$$

178 **2.2.4.2. Spoilage**

179 The inhibition of spoilage in strawberry in modified atmosphere is assumed to be the
180 result from inhibitory effect of gas composition on gas exchange in strawberry. When the
181 gas exchange is inhibited the overall metabolic rate and the ripening rate will be inhibited
182 resulting in a slower spoilage rate (Hertog et al., 1999). (Tijssens and Polderdijk, 1996)
183 used relative metabolic rate (equation 28), which represents a ratio of the actual
184 respiration rate under any gas conditions to the respiration rate under normal air
185 conditions (21% O₂, 0.03% CO₂) at the same temperature. In the case of strawberries

186 fermentative activities are taken into account in the respiration model therefore the gas
187 exchange is expressed in terms of CO₂ production.

$$188 \quad Rel_{MR} = \frac{r_{CO_2(f)}([O_2],[CO_2],[H_2O],T_s)}{r_{CO_2(21\% O_2,0.03\% CO_2,T_s)}} \quad (28)$$

189 The spoilage of strawberry due to *Botrytis*, in terms of percentage of strawberry affected
190 can be described by the following ordinary differential.

$$191 \quad \frac{dN}{dt} = Rel_{MR} \times k_s \times N \times \left(\frac{N_{max}-N}{N_{max}} \right), \text{ initiate at } N_0 \quad (29)$$

192 Where N_{max} is maximum spoilage (100%), k_s is the spoilage rate constant which depends
193 on the temperature according to Arrhenius equation. The value of activation energy
194 associated with the spoilage rate constant is mentioned in table 2.

195 **3. Numerical Simulations of the ODE system**

196 The mathematical model developed in the section above is used to estimate the effect of
197 input parameter uncertainty on the prediction of concentration of gases and effect on
198 waste generation during cold chain distribution. Stochastic simulations were performed
199 using three simulation scenarios to analyse the results of variability on strawberry cold
200 chain distribution.

201 1) A distribution scenario where temperature and relative humidity are varying
202 accordingly with the cold chain data described in (Joshi et al., 2018).

203 2) A distribution scenario with an ideal cold storage temperature (40 C). and relative
204 humidity (80%) and with variable product properties as specified in table 2.

205 3) A distribution scenario considering the joint uncertainties of 1) and 2).

206 The value of product parameters used in the model are in table 2. The ordinary
207 differential model was solved using the deSolve library (Soetaert et al., 2010) using the
208 *lsoda* solver on R 3.4.3 (R Development Core Team, 2008). All the plots were produced

209 using the ggplot2 library (Wickham, 2009). Sensitivity analysis using a main and first
210 order interactive effects model excluding time were analysed using a Lowry plot
211 (McNally et al., 2011).

212 **3.2. Uncertainty assessment**

213 **3.2.1. Assessment of cold chain on waste production**

214 The uncertainty in cold chain was expressed in changes temperature and relative
215 humidity. Figure 3.3 shows the temperature and relative humidity export cold chain
216 profile used for the study (Joshi et al. 2018). Figure 3.4 shows the retail cold chain profile
217 for temperature and relative humidity used for the study. The mathematical model was
218 simulated against these cold chain profiles to study the effect of cold chain uncertainty
219 on the quality of strawberry results are presented in section 5.3.1.

220 **3.2.2. Assessment of product variability on waste production**

221 The product parameters responsible for variability are presented in table 2 are simulated
222 at fixed cold chain profile of ideal storage temperature of 4⁰C and relative humidity 80%.

223 The results in following section show the uncertainty due to the product parameter
224 uncertainty on the quality parameters of strawberry causing waste in supply chain.

225 To further investigate the effect of individual product parameter, a sensitivity analysis
226 was performed using a main and first order interactive effects model excluding time. The
227 results are presented using a Lowry plot (McNally et al., 2011)

228 **3.2.3. Combined assessment of product and cold chain uncertainty effect on waste**

229 The combined assessment of cold chin uncertainty and product uncertainty was done to
230 understand which parameter is more influenced by which uncertainty and the
231 interventions that can be designed to maintain the quality and reduce waste in supply
232 chain. For further analysis, sensitivity analysis is done to access the effect of individual
233 parameter on quality explained in next section.

234 **3.3. Validation**

235 Strawberry (150g, 3-5 cm diameter) were purchased from local wholesale fruit market
236 Dublin, Ireland and packaged in an industry standard perforated polypropylene LDPE
237 film (4 perforations) and were stored in either ideal conditions (4⁰ C) or abuse condition
238 (1/2 day in packaging facility at 8 °C followed by transportation at 4 °C up to 2 days,
239 followed by retail storage including 4h at 20 °C, followed by 2 days at 8 °C, and finalised
240 by retail shop 4h at 20°C 2 days at 8 °C) for a period of 10 days.

241 A chitosan solution (1.5 %) was prepared by dissolving chitosan (Sigma-Aldrich Ltd.,
242 UK, medium molecular weight, 75-85% deacetylated) in distilled water containing 1%
243 glacial acetic acid using a magnetic stirrer. After complete dissolution 0.2% Tween 80
244 (Sigma-Aldrich Ltd., UK) was added to the solution. The pH of the solution was adjusted
245 to 5.2 with 1N NaOH (Sigma-Aldrich Ltd., UK) (Petriccione et al., 2015). A second
246 sample of the same batch of strawberries was immersed in chitosan solution for 60s then
247 allowed to dry for 1 hour in air dryer at room temperature and stored in the same
248 conditions as above.

249 Strawberries were visually examined on regular intervals during storage period. The fruits
250 showed surface mycelia growth or bacterial lesions were considered decay. Results were
251 expressed as percentage of spoiled fruits. Weight loss was expressed as percentage loss
252 of initial weight (Han et al., 2004).34.

253 **Results and discussions**

254 **4.1. Cold chain variability assessment**

255 The mathematical model in section 2 was used to simulate the effect of cold chain
256 variation to predict the changes in the concentration of gases in the headspace and quality
257 of strawberry against the export cold chain profile. The governing ODE equations (5 and
258 6) were used to obtain the concentration of carbon dioxide and oxygen in the headspace

259 of package. The results presented in Fig 1 were simulated along with the export cold
260 chain. It can be seen how the creation and maintenance of optimal atmosphere inside
261 modified atmosphere package depends on the respiration rate of the product and on the
262 permeability of the films both of which are dependent on temperature. At very low oxygen
263 concentration (<2%) anaerobic respiration is initiated in the tissue which shortens the
264 shelf life. The results obtained from the simulations showed there was no anaerobic
265 condition observed in the package.

266 Temperature fluctuation and their effect on the atmosphere inside the package have a
267 major effect on the quality of strawberry. The spoilage of strawberry increases with
268 increase in temperature, however the effect of MA was evident on the package. A linear
269 effect of concentration of CO₂ is observed on the spoilage. At 0% CO₂, 1.72 % spoilage
270 is observed to 0.87% spoilage at 18 % CO₂ (Kader, 1986). At higher concentration of CO₂
271 (20-80%) clear inhibition was observed. At these extremely high level of CO₂ fungal
272 growth is inhibited in strawberries (Ke et al., 1991). The amount of water vapour in the
273 headspace of the package is estimated using Fick's diffusion and psychometric equations,
274 this was used to calculate relative humidity inside the package. The results obtained
275 showed the package water vapour pressure was saturated (RH=100%) during storage.
276 (Fishman et al., 1996) obtained similar results for MAP of mango, and (Song et al., 2002)
277 obtained similar experimental and predicted results of relative humidity saturating rapidly
278 during storage.

279 Weight loss as a result of transpiration and carbon loss due to respiration was directly
280 dependent on the temperature (Fig 1 (c)). Sanz et al., (2000) reported weight loss of 3.53%
281 in control packages and 0.9% in micro-perforated packages towards the end of storage (7
282 days). The barrier in the movement of water vapour through the film and perforations
283 leads to less weight loss. The spoilage of strawberry increases with increase in

284 temperature Fig 1. However the effect of MA was evident on the package. The spike in
285 spoilage (>5%) after 2 days of storage was due to the result of abusive temperature profile.
286 A linear effect of concentration of CO₂ was observed on the spoilage, at 0% CO₂ 1.72 %
287 spoilage was observed to 0.87% spoilage at 18 % CO₂ (Kader, 1986). At higher
288 concentration of CO₂ (20-80%) clear inhibition of spoilage was observed. At these
289 extremely high level of CO₂ fungal growth was inhibited in strawberries (Ke et al., 1991).

290 **4.2. Product variability assessment**

291 Knowledge of biological variation in quality within batch is important in managing
292 uniform quality within cold chain. It could help predict the factors responsible for
293 deterioration of quality during storage. The model developed in this scenario study can
294 help find the effect of product variability on the fate of quality and waste generation
295 (Hertog et al., 1999). The results obtained are the estimates of the values expected due to
296 variability in product parameters. Fig 2 shows the propagation of product parameters on
297 the quality characteristics of strawberry at different storage temperature (4, 20 and 8⁰ C).
298 It is evident from the figure the variation was directly dependant on the temperature,
299 higher the temperature higher is the variation associated with it.

300 $V_{m_{O_2,ref}}$ and $V_{m_{CO_2(f)ref}}$ are the respiration rate parameters which are directly dependant
301 on temperature. The increase in temperature resulted in increase in the respiration rate.
302 (Geysen et al., 2005) mentioned the effect of temperature on the activation energy of
303 maximum O₂ consumption. Weight loss of strawberry constantly increased with time,
304 with a higher weight loss being observed at higher temperature. Strawberries have no
305 protective skin their skin mass transfer coefficient (Ks) is significantly higher than other
306 commodities, which leads to higher weight loss due to transpiration. There is less
307 uncertainty seen in weight loss due to the product parameters. As the storage temperature
308 increased the variability also increased as evident in figure 2(c). At 40C the weight loss

309 was less than 0.5% in 10 days whereas at 200C the 2.7% weight loss was observed.
310 Spoilage increased with increases of storage temperature as evident from figure 5.3(d).
311 At 40C the spoilage observed was less than 15% in 10 days storage, at 80C the spoilage
312 of around 37% was observed and at 200C 100% spoilage was seen in 6 storage days. The
313 effect of CO₂ on spoilage could be explained by the effect of CO₂ on the respiration rate.
314 Hertog showed that *Botrytis* inoculated strawberry displayed an inhibitory effect of CO₂
315 on spoilage levels below 20%, which was strongly batch dependant (Hertog et al., 1999).

316 **4.3. Comparing the effect of variability on quality of strawberry**

317 The uncertainty associated with cold chain variability (temperature and relative humidity)
318 and the variation associated with biological product parameters was compared by plotting
319 kernel density plots for each food chain distribution day and for each of the scenarios. Fig
320 3 (a) and (b) show how the concentration of gases in the headspace of package was
321 dependent both on cold chain and product variability. The second peak observed in the
322 figure is the result of abusive storage temperature (>10⁰C). Variation at the 4th day of
323 distribution in CO₂ and O₂ seems to be largely cold chain dependent, however by day 6
324 the cold chain variation has reduced below the variation of the product.

325 Weight loss in strawberry showed dependence on the cold chain factors, temperature and
326 relative humidity of storage. Strawberry stored at 10 C showed less than 1% weight loss
327 in 8 days whereas at 200 C 8% weight loss was observed in 4 days which is above the
328 acceptable limit (Nunes et al., 1998). The spoilage of strawberry (Fig 3(d)) showed more
329 influence by the cold chain factors at the beginning of the cold distribution but product
330 uncertainty had more prominent influence later during storage. Strawberries have been
331 found to be colonised by the fungus *B. cinerea* before packaging, with the fungal infection
332 increasing with storage time and inadequate storage conditions (Almenar et al., 2007).
333 The initial spoilage (N₀) is a value representing initial ripening stage or sensitivity of

334 strawberry to botrytis infection (Hertog et al., 1999). From fig 3(c) and (d) it is evident
335 that to control weight loss variation the cold chain conditions (temperature and relative
336 humidity) needed to be controlled whereas in case of spoilage product parameters are the
337 main cause of variability and need to be controlled to maintain the shelf life.

338 **4.4. Sensitivity Analysis**

339 Sensitivity analysis was performed to study the results of variation and how it could be
340 apportioned qualitatively and quantitatively to different sources of variation in the model
341 input (Kader, 1984) The result of the sensitivity analysis (SA) on the weight loss of
342 packed strawberry is presented in Fig 4 (a). The most important parameters contributing
343 to the 90% of the variability were a combination of respiration rate parameters
344 (RQ_{ox} , $Vm_{O_2,ref}$, K_{mO_2}), skin mass transfer coefficient (K_s) and the activation energies
345 associated with ($E_{aVm_{O_2}}$, $E_{aVm_{CO_2(f)}}$). It was also a combination of main effect of the
346 product parameters and their interactive effects. This suggests that controlling the
347 respiration rate of fresh produce and reducing the mass transfer through skin will help
348 reduce losses during supply chain.

349 *Identification of an effective intervention*

350 The result of sensitivity analysis of spoilage of strawberry shows that the most important
351 parameters contributing to 90% of variability were the initial spoilage and spoilage rate
352 constant ($k_{s,ref}$) (Fig 4(b)). Thus, the waste due to spoilage could be reduced by
353 controlling the initial quality of strawberry and the spoilage rate. The product parameters
354 contributing to the concentration of CO_2 in the headspace of packaging were
355 $Vm_{O_2,ref}$, RQ_{ox} and $E_{Vm_{O_2,ref}}$. Those contributed to the 90% of the variability thus
356 controlling respiration would aid to reduce the waste produced in the supply chain.

357 **4.5. Validation experiment**

358 The input model parameters from table 2 and 3 are used to compare the experimental and
359 predicted results presented in the fig. 5. The experiments were performed to simulate real
360 life abusive supply chain conditions for 10 days. Weight loss, colour, firmness and
361 spoilage were measured at 1, 3, 5, 7 and 10th day. The grey ribbon represents the
362 uncertainty margins of 5% and 95% percentiles due to variability in the simulations of
363 these conditions.

364 The results for weight loss showed that the variability associated with the product
365 parameter was not high (fig 2(c)). Cold chain parameters were responsible for the
366 variability caused for weight loss during the distribution chain of strawberry.

367 Spoilage showed high product variability which increased with increases in storage
368 temperature (fig. 2(d)). The experimental results fell within the grey ribbon pertaining to
369 the variability associated with it (Fig 5(d)).

370 **4.6. Waste estimation during supply chain**

371 Fig 6 show the total waste estimation throughout the supply chain, as a combination of
372 waste due to weight loss and the spoilage for coated and uncoated strawberries. Threshold
373 values were used to calculate the waste (weight loss of 5% or above which it starts
374 shrivelling and becomes unmarketable) and 5% for strawberry spoilage. It can be seen
375 how significant amounts of out-of-specification product yielding finally to waste start
376 appearing in day 2 of distribution and that by the end of day 3 there was approximately
377 10% of all product potentially on a course of not being suitable for consumption and
378 yielding to waste due to variability in the product and cold chain conditions reflecting on
379 the weight loss and spoilage..

380 **5. Conclusions**

381 A mathematical model was developed to predict the changes in quality of packed
382 strawberry during distribution. It took into account the heat and mass transfer processes
383 taking place in MAP like respiration, transpiration condensation and transport of these
384 gases through permeable film. The kinetic behaviour of fresh produce was modelled with
385 respect to the cold chain condition and product parameter. The effect of cold chain
386 variability and product variability on the quality of fresh produce was assessed. Weight
387 loss was influenced by the cold chain factors whereas spoilage has initial influence from
388 cold chain factors but product variability becomes prominent towards end of storage. The
389 results of sensitivity analysis showed that controlling respiration rate and skin mass
390 transfer would help reduce the waste produced during supply chain. This mathematical
391 model contributed to assessing the factors responsible for spoilage and designing
392 strategies to reduce waste produced in cold supply chain.

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395 Development Plan 2007-2013, through the Food Institutional Research Measure,
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517

518

Process	Equation	Reference	Eq. no.
Respiration	$r_{O_2} = \frac{vm_{O_2} \cdot [O_2]}{Km_{O_2} \cdot \left(1 + \frac{[CO_2]}{Kmc_{CO_2}}\right) + [O_2] \cdot \left(1 + \frac{[CO_2]}{Kmu_{CO_2}}\right)}$	Strawberry respiration rate follow uncompetitive type inhibition. The CO ₂ production is a combination of oxidative and the fermentative process (Hertog et al., 1999; Song et al., 2002)	(1)
	$r_{CO_2(f)} = \frac{vm_{CO_2(f)}}{\left(1 + \frac{[O_2]}{Kmc_{O_2(f)}} + \frac{[CO_2]}{Kmc_{CO_2(f)}}\right) \cdot Km_{CO_2(f)} + 1}$		(2)
	$r_{CO_2} = RQ_{ox} \cdot r_{O_2} + r_{CO_2(f)}$		(3)
Respiration heat	$Q_s = \frac{2816}{6} \times \frac{r_{O_2} + r_{CO_2}}{2} \times \alpha \times W_p$	α is conversion factor of respiration energy dissipated as heat. The literature suggests the value of α has a range between 0.8-1.0 (Burton, 1982). For 100% conversion of respiration energy as heat $\alpha = 1$ (Song et al., 2002)	(4)
Mass Balance			
Gas exchange in package	$\frac{d[O_2]_i}{dt} = 100 \times \left(\frac{A_p P_{O_2} P_{atm}}{L_f} \left[\frac{[O_2]_o}{100} - \frac{[O_2]_i}{100} \right] - W_p r_{O_2} \right) \times \frac{1}{V_f}$	The mass balance of gas components in the package is represented by ordinary differential equations (Song et al., 2002). As the package initially contains air, initial conditions (t=0) becomes $[O_2]_i = 21.0\%$, $[CO_2]_i = 0.03\%$	(5)
	$\frac{d[CO_2]_i}{dt} = 100 \times \left(\frac{A_p P_{CO_2} P_{atm}}{L_f} \left[\frac{[CO_2]_o}{100} - \frac{[CO_2]_i}{100} \right] + W_s r_{CO_2} \right) \times \frac{1}{V_f}$		(6)
Permeability	$P_{O_2, CO_2, H_2O} = P_{O_2, CO_2, H_2O \text{ ref}} + \frac{\pi R_h^2 \times D_{i, air}}{(L_f + R_h)} \times N_h$	Permeability is a function of permeability of film and the number and size of perforations.	(7)

Water permeation through film	$\frac{dm_{pr}}{dt} = \left[\frac{P_{H_2O} A_p (P_i - P_o)}{L_f} \right] \left[\frac{0.018 P_{atm}}{RT_s} \right]$	The driving force of permeation of water vapour from the headspace of package to surrounding is the water vapour pressure difference.	(8)
Heat Balance			
Temperature headspace of package	$Q_s W_s + Q_{con} + h_p A_p (T_i - T_o)$ $= Q_{tr} + W_s C_s \frac{dT_s}{dt} + W_a C_a \frac{dT_s}{dt}$ $\frac{dT_s}{dt} = \frac{Q_r + Q_{con} - h_p A_p (T_i - T_o) - Q_{tr}}{W_s C_s + W_a C_a}$	The heat is generated by respiration and heat is transferred in headspace due to convection, transpiration and condensation. This ODE is used to estimate the temperature of the fresh produce (Lee et al., 1996)	(9)
			(10)

521

522 **Table 2 Parameter estimate and their standard error for strawberry** Source:

523 (*Becker et al., 1996; Hertog et al., 1999)

Parameter	Value	Standard error (SE)
$Vm_{O_2,ref}$ ($\mu\text{mol kg}^{-1}\text{sec}^{-1}$)	0.27	0.010
$E_{aVm_{O_2}}$ (J mol^{-1})	74826	3451
$Vm_{CO_2(f)ref}$ ($\mu\text{mol kg}^{-1}\text{sec}^{-1}$)	0.50	0.22
$E_{aVm_{CO_2(f)}}$ (J mol^{-1})	57374	14400
Km_{O_2} (%)	2.63	0.274
Km_{CO_2}	$+\infty$	-
Kmu_{CO_2}	$+\infty$	-
$Km_{CO_2(f)}$ (%)	0.056	0.041
$Km_{CO_2(f)}$	$+\infty$	-
$Km_{CO_2(f)}$ (%)	1	-
K_s^* ($\text{kg m}^{-2} \text{sec Pa}$)	13.6×10^{-9}	4.8
$k_{s,ref}$ (day^{-1})	0.60	0.045
Ea_s (J mol^{-1})	70108	7056
N_0 (%)	0.83	0.10

524

525 **Table 3 Properties of packaging film, produce and other conditions used in the**

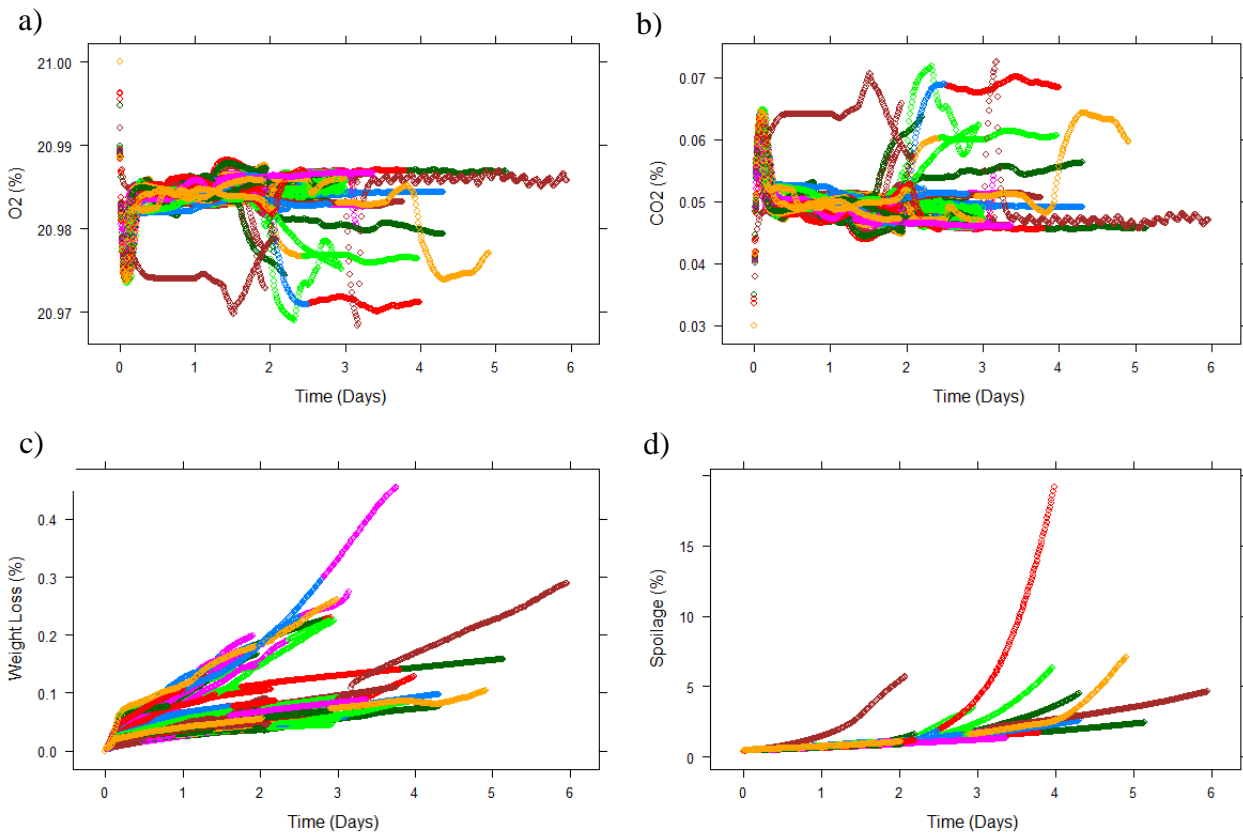
526 **model**

$P_{O_2 ref}$ ($\text{m}^3\text{m h}^{-1}\text{m}^{-2}\text{Pa}$)	8.5×10^{-14}	(Xanthopoulos et al., 2012)
$P_{CO_2 ref}$ ($\text{m}^3\text{m h}^{-1}\text{m}^{-2}\text{Pa}$)	2.8×10^{-13}	(Xanthopoulos et al., 2012)
$P_{H_2O ref}$ ($\text{m}^3\text{m h}^{-1}\text{m}^{-2}\text{Pa}$)	4.5×10^{-13}	(Xanthopoulos et al., 2012)
ρ_b (kg m^{-3})	600	(Xanthopoulos et al., 2012)
ϵ	0.27	(Xanthopoulos et al., 2012)
a_w	0.99	(Xanthopoulos et al., 2012)
C_s ($\text{kJ kg}^{-1} \text{K}^{-1}$)	4	(ASHRAE, 2006)
$[CO_2]_i$ (%)	0.03	(Song et al., 2002)
$[O_2]_i$ (%)	21.0	(Song et al., 2002)
M_{O_2} (kg mol^{-1})	0.032	(Bird, 2002)
M_{CO_2} (kg mol^{-1})	0.044	(Bird, 2002)
M_{H_2O} (kg mol^{-1})	0.018	(Bird, 2002)
R ($\text{J K}^{-1}\text{mol}^{-1}$)	8.314	(Bird, 2002)
P_{atm} (Pa)	101325	(Bird, 2002)
ρ_{O_2} (kg m^{-3})	1.43	(Siracusa, 2012)

ρ_{CO_2} (kg m ⁻³)	1.98	(Siracusa, 2012)
T_{ref} (°C)	10	(Hertog et al., 1999)
N_H	4	Experimental
d_c (m)	0.03	Experimental

527

528



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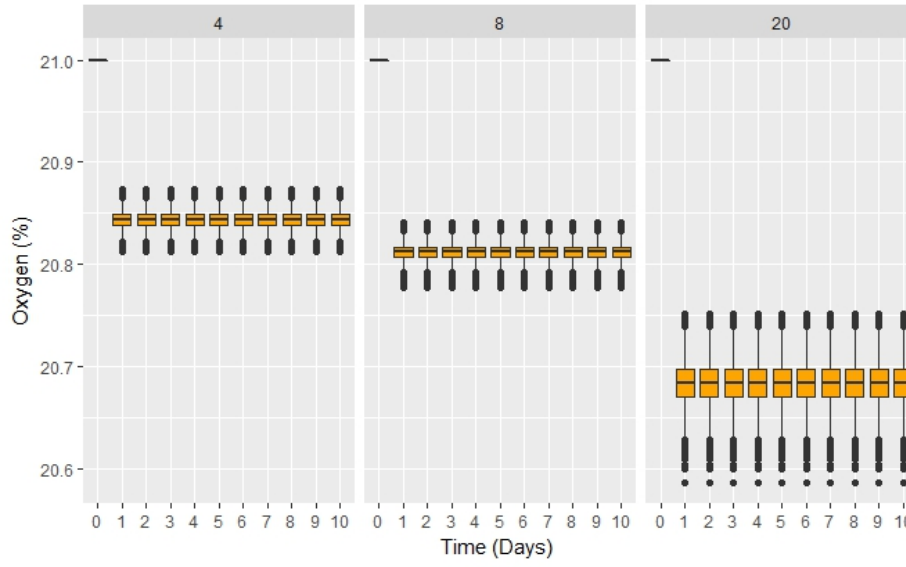
530 **Fig 1. Simulation results of average (a) oxygen concentration and (b) carbon dioxide**
 531 **concentration in the headspace of packages (c) weight loss observed and (d) spoilage**
 532 **against the cold chain profile.**

533

534

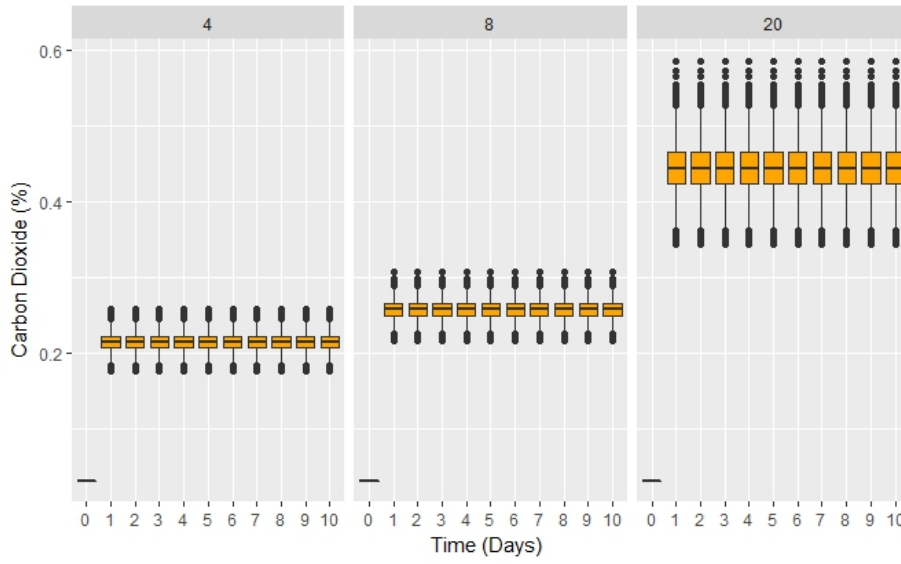
535

a)



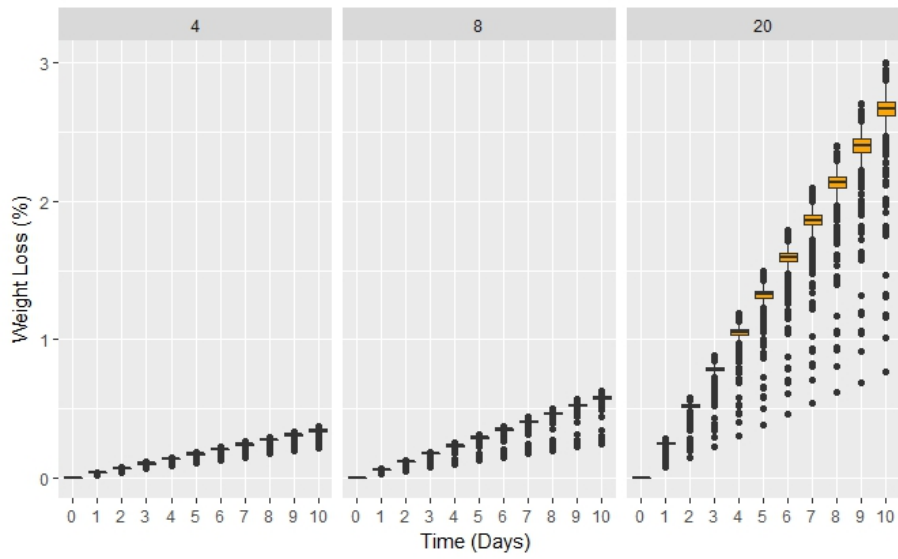
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b)

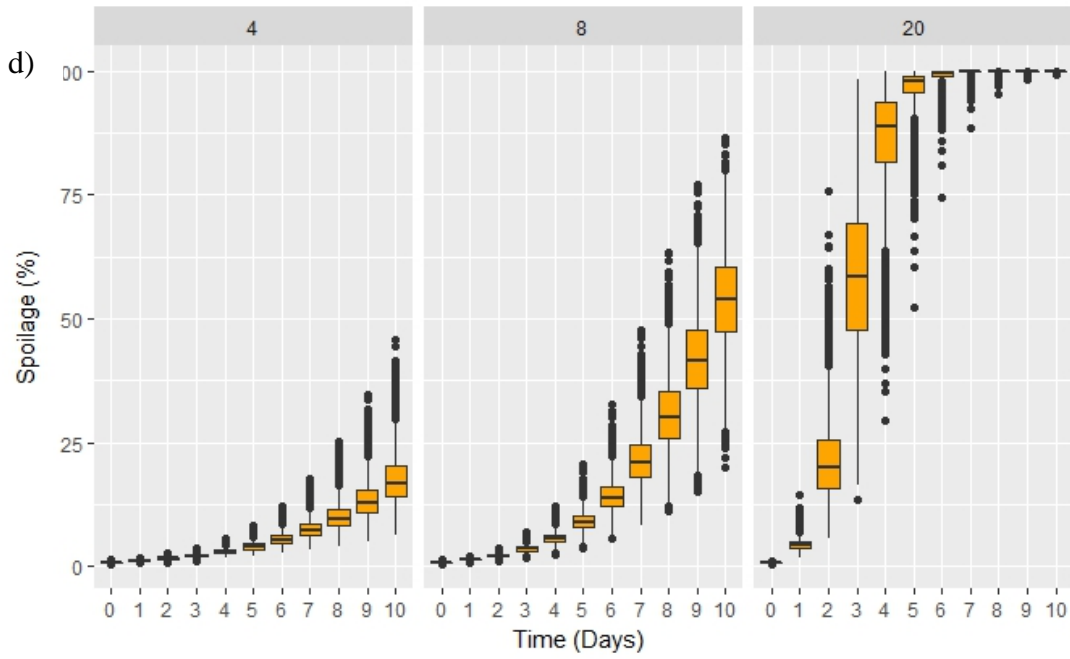


537

c)



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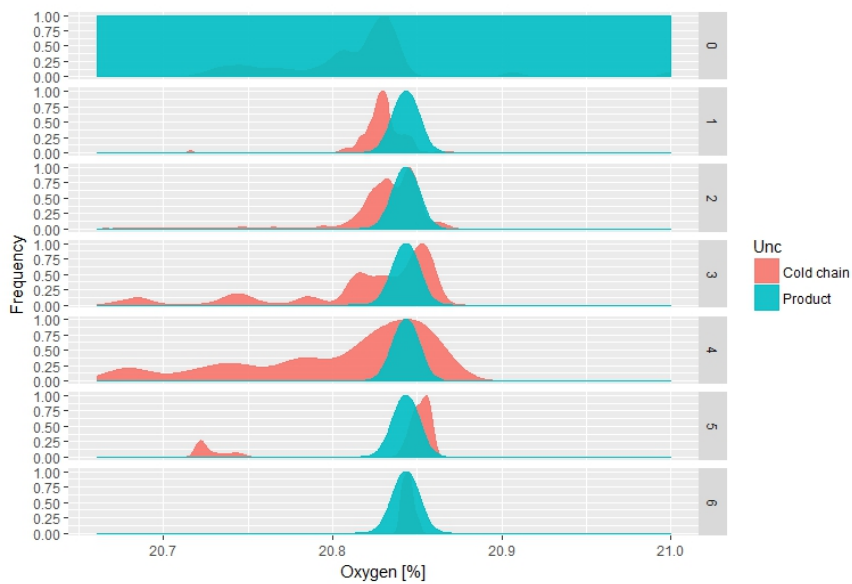
539

540 **Fig 2 Propagation of product parameter variability observed in (a) concentration of**
 541 **oxygen (b) carbon dioxide in headspace (c) weight loss and (d) Spoilage observed in**
 542 **strawberry packed in modified atmosphere 15 days storage at 4° C and 80% RH.**

543

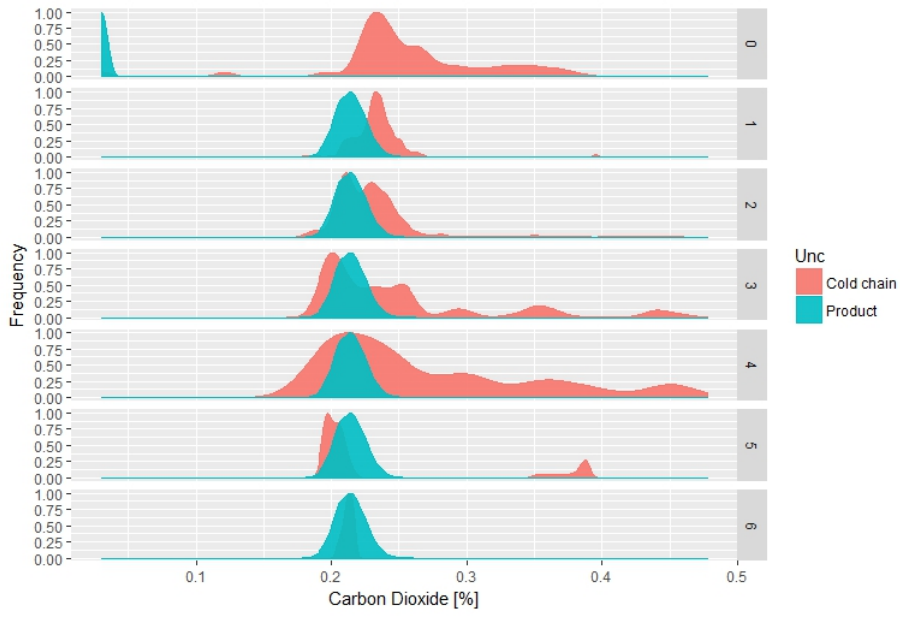
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a)



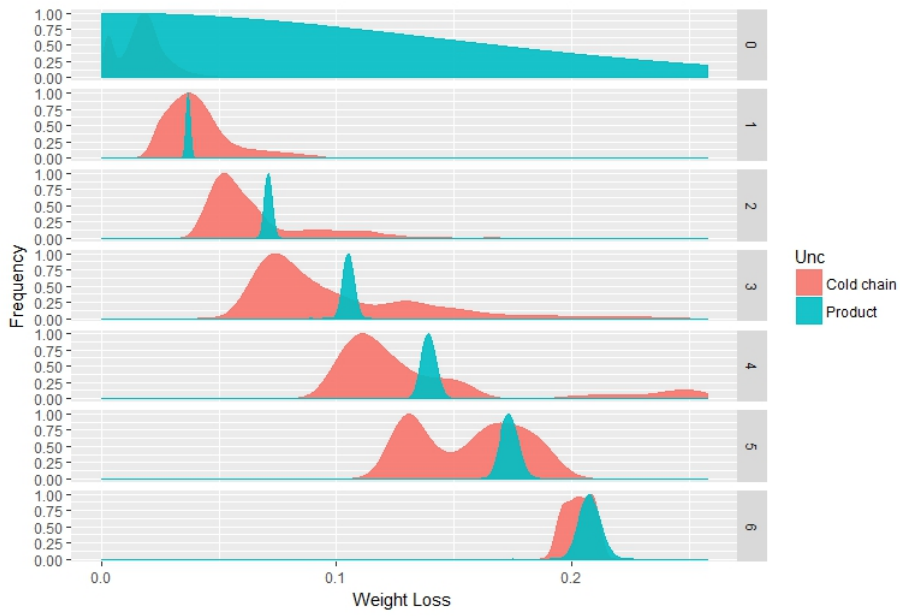
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b)



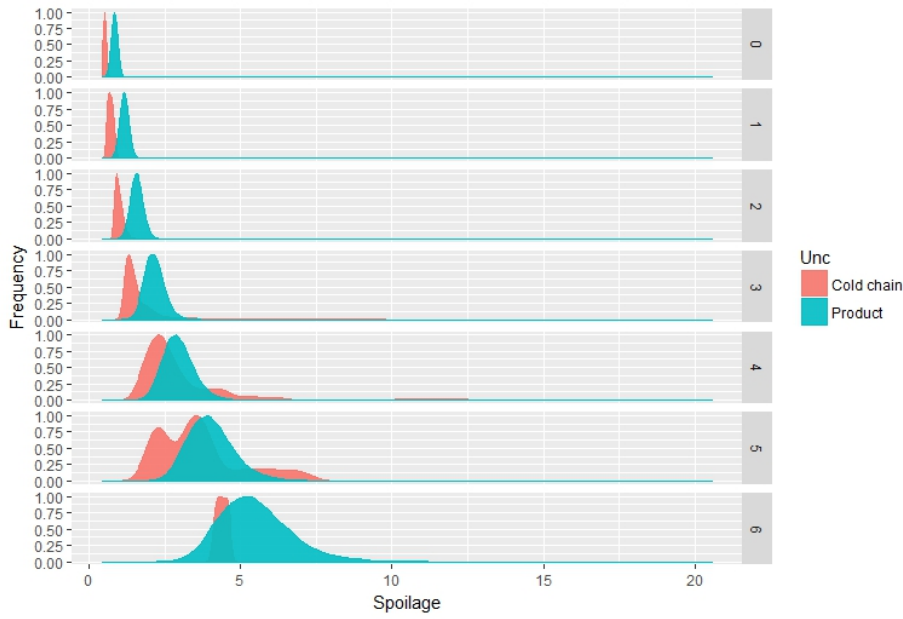
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c)



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d)

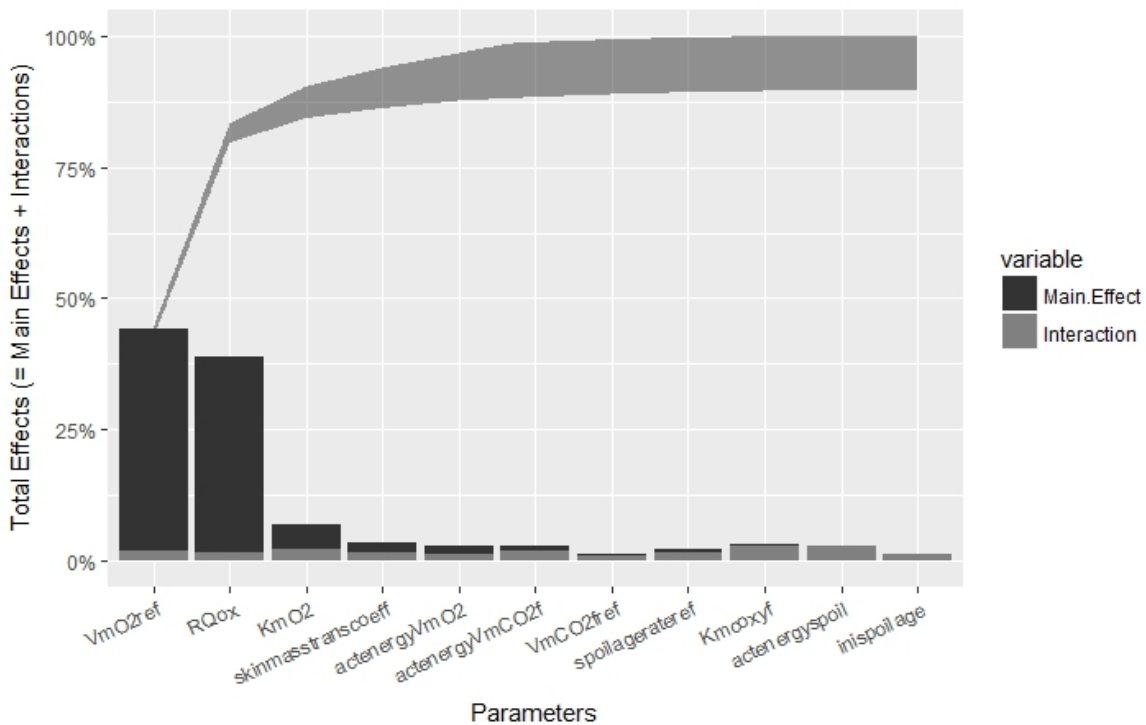


548

549 **Fig 3 The effect of cold chain uncertainty (green) and product parameter**
 550 **uncertainty (orange) on the (a) oxygen concentration (b) carbon dioxide**
 551 **concentration in headspace (c) weight loss during storage (d) Spoilage of strawberry.**
 552 **Each subplot within (a), (b), (c) and (d) represents the simulated variation in a given**
 553 **distribution day**

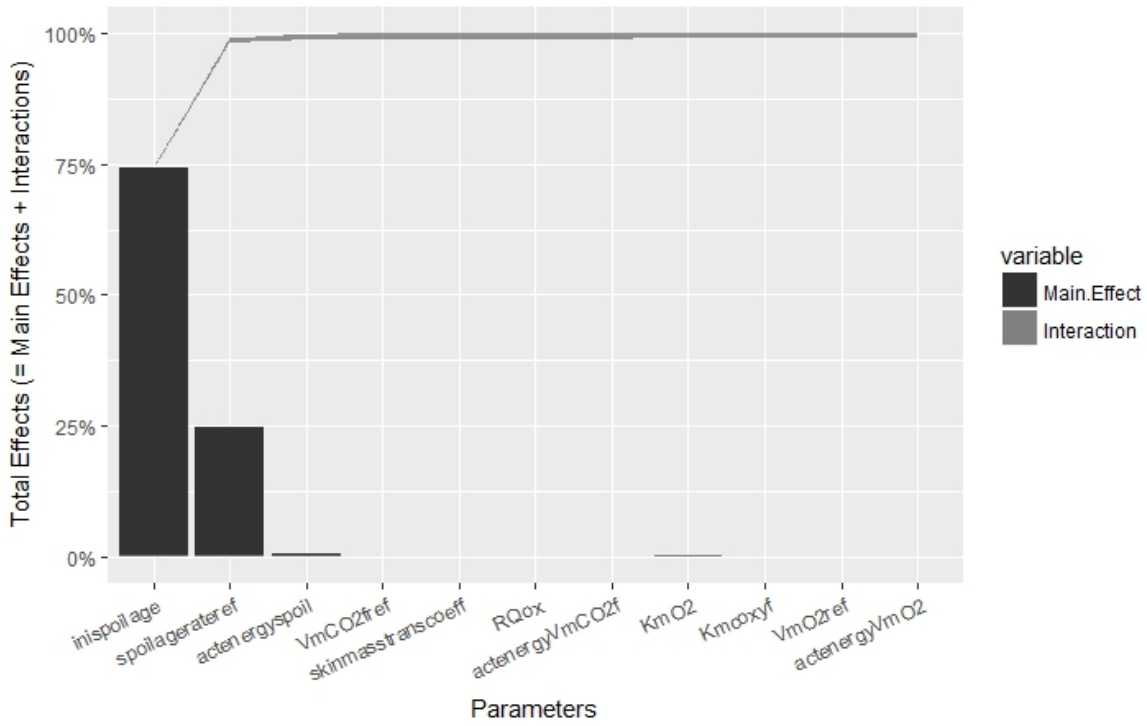
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a)



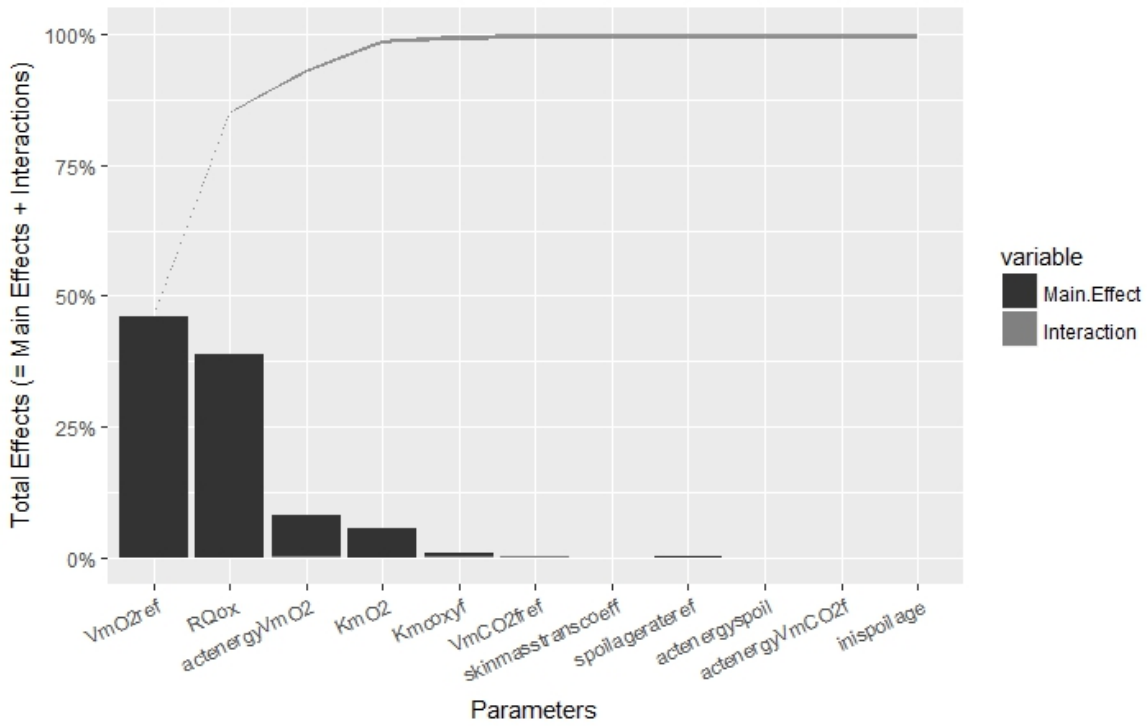
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b)



556

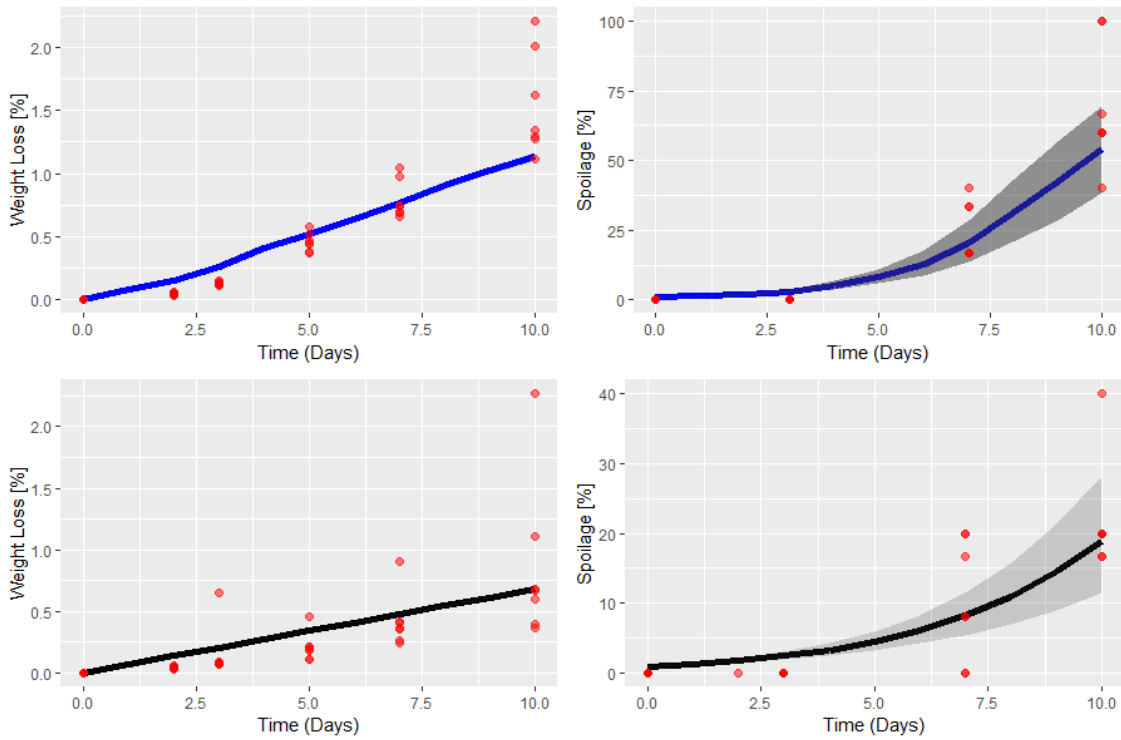
c)



557

558 **Fig. 4** Lowry plot for the effect of product parameters on the a) weight loss b)

559 **spoilage, c) CO₂**



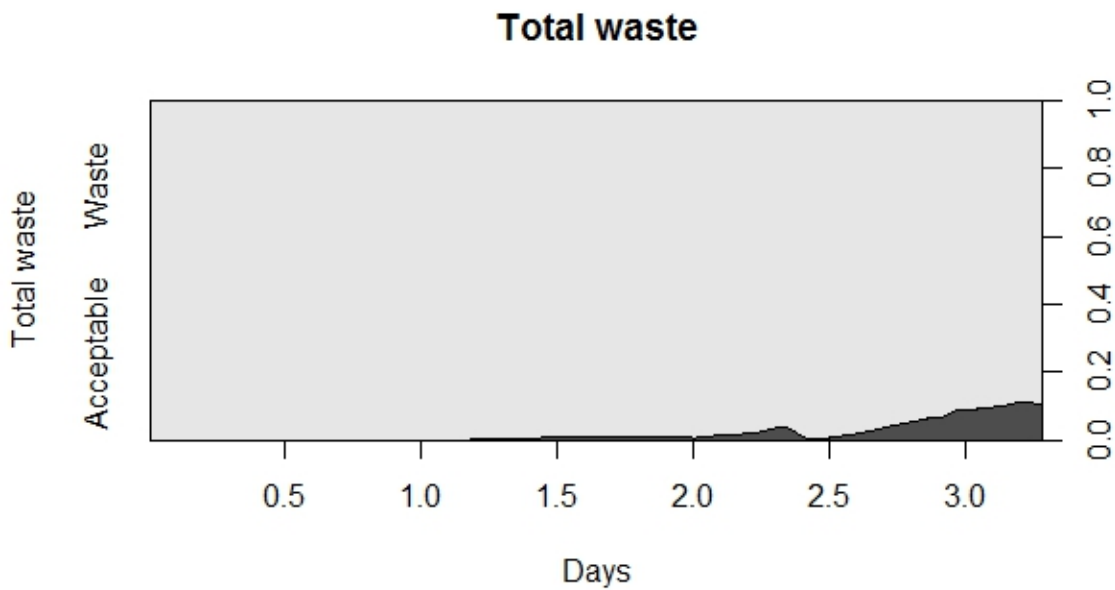
560

561 **Fig. 5 Comparison of model predictions with the experimental data (points) at**

562 **different storage conditions ((4, 8, 20⁰ C) (a, b) and at ideal temperature (4⁰C) (c,d)**

563 **a) weight loss b) spoilage at (4, 8, 20⁰ C) , c) weight loss and d) spoilage at (4⁰C).**

564



565

566 **Fig. 6 Conditional density plot of total waste generated in the strawberry supply**
567 **chain.**